

# Radiative Heat Transfer in a Utility Boiler

# Introduction

In recent years, many studies have been conducted in the field of performance optimization of large power plant boilers. The main aims have been to extend the lifetime, increase the thermal efficiency, and reduce the pollutant emissions of the boilers. A good furnace design is the most important part in the energy conversion process in the boilers. A furnace is where the fuel is burnt and the chemical energy is converted into heat to be transferred into the water walls of steam boilers. The temperatures in fuel furnaces are high enough that the radiation becomes the most important mechanism in heat transfer. Due to complexity of the radiation mechanism and its dependence on the enclosure's geometry, there is no analytical solution except for very simple problems. This fact along with expensive experimental modeling leads researchers to develop numerical models for analyzing these enclosures. Three of the most attractive methods, as far as accuracy and computational requirement are concerned, are the discrete transfer, the discrete ordinates and the finite-volume methods.

Note: Solving this application requires approximately 7 GB of memory.

# Model Definition

Of practical relevance is the radiative heat transfer in furnaces containing obstacles, such as protrusions and obstructions. In some applications, the thickness of the obstacles is very small as it occurs in utility boilers, where panels are often hanged in the radiation chamber.

In order to reduce the mesh (and then the computational cost), these obstructions are modeled as baffles (zero thickness). This study handles zero thickness obstacles containing an emitting-absorbing medium.

A three-dimensional enclosure resembling the combustion chamber of a utility boiler is modeled. The enclosure contains five baffles, as shown in Figure 1, which simulates the panels of superheaters suspended at the top of the combustion chamber.



Figure 1: Utility boiler with obstructions.

In this example, the S4 discrete ordinate method was employed for predicting the heat flux on the side walls of enclosures and incident radiation distribution within the furnace. It results in a set of 24 discrete directions to represent radiative intensity transport.

The main assumption is using an existing uniform temperature and properties within the volume and surface zones, as proposed in Ref. 1. The temperature and emissivity of the boundaries, including the surface of the baffles, are taken as 800 K and 0.65, respectively, except at x = 10 m and for  $22 \le z \le 30$  m, where the temperature was set equal to 1200 K and a blackbody surface is assumed. An emitting-absorbing medium is assumed, with the following distribution of temperature and absorption coefficient:

Coordinate (m)	Absorption coefficient (1/m)	Temperature (K)		
z ≤ 5	0.20	1600		
5 < z ≤ 10	0.25	2000		

TABLE I: DISTRIBUTION OF TEMPERATURE AND ABSORPTION COEFFICIENT.

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Coordinate (m)	Absorption coefficient (1/m)	Temperature (K)		
10 < z ≤ 20	0.20	1600		
$20 < z \leq 30$	0.18	1200		

#### THERMAL ANALYSIS

The discrete-ordinates method (DOM) relies on the discrete representation of the directional dependence of the radiation intensity. The radiative transfer equation (RTE) is solved for a set of discrete directions,  $s_i$ , which span the total solid angle range of  $4\pi$  around a point in space.

The RTE for this type of configuration can be written as:

$$s \cdot \nabla I(r,s) = \kappa I_{\rm b}(T) - \beta I(r,s) + \frac{\sigma_{\rm s}}{4\pi} \int_0^{4\pi} I(r,s') \phi(r,s',s) d\Omega'$$

where

- I(r, s) is the radiative intensity at a given position r, following s direction
- *T* is the temperature
- $\kappa$ ,  $\beta$ ,  $\sigma_s$  are absorption, extinction, and scattering coefficients, respectively
- $I_{\rm b}(T)$  is the blackbody radiative intensity
- φ(r, s', s) is the scattering function. φ(r, s', s) = 1 + α<sub>1</sub>μ<sub>0</sub> and μ<sub>0</sub> = s' · s is the cosine of the scattering angle.

The boundary intensities in the furnace walls are given physically by the effective emitted intensity plus reflected incident intensities into a respective direction.

$$I_{\rm bnd}(r,s) = \varepsilon_{\rm w} I_{\rm b}(T) + \frac{\rho_{\rm d}}{\pi} q_{\rm out} \quad \text{ for all } s \text{ such that } \mathbf{n} \cdot s < 0$$

where

- $\varepsilon_w$  is the surface emissivity, which is in the range [0, 1]
- $\rho_d = 1 \varepsilon_w$  is the diffusive reflectivity
- **n** is the outward normal vector
- q<sub>out</sub> is the heat flux striking the wall:

$$q_{\text{out}} = \int_{(\mathbf{n} \cdot s' > 0)} (\mathbf{n} \cdot s') I(r, s') d\Omega'$$

The above equations can be discretized in Cartesian coordinates for monochromatic or gray radiation as

$$s_i \cdot \nabla I_i = \kappa I_{\rm b}(T) - \beta I_i + \frac{\sigma_{\rm s}}{4\pi} \int_0^{4\pi} I(r,s') \phi(r,s',s) d\Omega'$$

The Sn approximation of the RTE in the m direction can be expressed as

$$s_i \cdot \nabla I_i = \kappa I_{\mathbf{b}}(T) - \beta I_i + \frac{\sigma_{\mathbf{s}}}{4\pi} \sum_{j=1}^n w_j I_j \phi(r, s_j, s_i)$$

For a discrete direction,  $s_i$ , the values of  $s_{i,1}$ ,  $s_{i,2}$ , and  $s_{i,3}$  define the direction cosines of  $s_i$  obeying the condition  $s_{i,1}^2 + s_{i,2}^2 + s_{i,3}^2 = 1$ . The *j* index in the above equation denotes the direction of incoming radiation contributing to the direction  $s_i$ .

For a diffuse reflecting surface on a wall boundary, the boundary condition equation is transformed as

$$I_{i, \text{bnd}} = \varepsilon_{w}I_{b}(T) + \frac{\rho_{d}}{\pi} \sum_{(\mathbf{n} \cdot s_{j} > 0)} w_{j}I_{j}(\mathbf{n} \cdot s_{j}) \quad \text{for all } s_{i} \text{ such that } \mathbf{n} \cdot s_{i} < 0$$

# Results and Discussion

Figure 2 and Figure 3 show the predicted incident radiation surface plots. The maximum incident radiation occurs at the level where the temperature and absorbing coefficient of the medium are the highest (that is, at the boiler's burner level).



Figure 2: Incident radiation.



Figure 3: Incident radiation on the front of the boiler  $(W/m^2)$ .



The predicted outgoing heat flux is shown in Figure 4 and is in good agreement with published data (Ref. 1).

Figure 4: Outgoing heat flux on walls of the boiler  $(W/m^2)$ .

# Reference

1. P.J. Coelho, J.M. Goncalves, and M.G. Carvalho, "Modelling of Radiative Heat Transfer in Enclosures with Obstacles," *Int'l J. Heat and Mass Transfer*, vol. 41, no. 4– 5, pp. 745–756, 1998.

Application Library path: Heat\_Transfer\_Module/Thermal\_Radiation/boiler

# Modeling Instructions

From the File menu, choose New.

NEW

In the New window, click 🙆 Model Wizard.

#### MODEL WIZARD

- I In the Model Wizard window, click 间 3D.
- 2 In the Select Physics tree, select Heat Transfer>Radiation> Radiation in Participating Media (rpm).
- 3 Click Add.
- 4 Click  $\bigcirc$  Study.
- 5 In the Select Study tree, select General Studies>Stationary.
- 6 Click **M** Done.

#### GLOBAL DEFINITIONS

#### Parameters 1

- I In the Model Builder window, under Global Definitions click Parameters I.
- 2 In the Settings window for Parameters, locate the Parameters section.
- **3** In the table, enter the following settings:

Name	Expression	Value	Description
Thot	1200[K]	1200 K	Temperature, hot surface zone
Tlow	800[K]	800 K	Temperature, cool surfaces
em	0.65	0.65	Emissivity, cool surfaces
scattC	O[1/m]	0 I/m	Scattering coefficient

#### Piecewise I (pwI)

- I In the Home toolbar, click f(X) Functions and choose Global>Piecewise.
- 2 In the Settings window for Piecewise, type T in the Function name text field.
- **3** Locate the **Definition** section. In the **Argument** text field, type z.
- 4 Find the Intervals subsection. In the table, enter the following settings:

Start	End	Function
0	5	1600
5	10	2000
10	20	1600
20	30	1200

5 Locate the Units section. In the Arguments text field, type m.

6 In the Function text field, type K.

Piecewise 2 (pw2)

I In the Home toolbar, click f(X) Functions and choose Global>Piecewise.

2 In the Settings window for Piecewise, type absC in the Function name text field.

**3** Locate the **Definition** section. In the **Argument** text field, type z.

**4** Find the **Intervals** subsection. In the table, enter the following settings:

Start	End	Function
0	5	0.20
5	10	0.25
10	20	0.20
20	30	0.18

5 Locate the Units section. In the Arguments text field, type m.

6 In the Function text field, type 1/m.

## GEOMETRY I

Work Plane I (wp1)

- I In the Geometry toolbar, click 📥 Work Plane.
- 2 In the Settings window for Work Plane, locate the Plane Definition section.
- 3 From the Plane list, choose xz-plane.
- 4 Click 🖄 Go to Plane Geometry.

Work Plane I (wp1)>Polygon I (pol1)

- I In the Work Plane toolbar, click / Polygon.
- 2 In the Settings window for Polygon, locate the Coordinates section.
- 3 From the Data source list, choose Vectors.
- **4** In the **xw** text field, type 0 0 0 10 10 10 10 8 8 10 10 10 10 6 6 4 4 0.
- 5 In the yw text field, type 4 30 30 30 30 22 22 20 20 18 18 4 4 0 0 0 0 4.
- 6 In the Work Plane toolbar, click 🏢 Build All.

Work Plane I (wp1)>Rectangle I (r1)

- I In the Work Plane toolbar, click 📃 Rectangle.
- 2 In the Settings window for Rectangle, locate the Size and Shape section.
- 3 In the Width text field, type 4.
- 4 In the **Height** text field, type 10.

- 5 Locate the **Position** section. In the **yw** text field, type 20.
- 6 In the Work Plane toolbar, click 🟢 Build All.

#### Extrude I (extI)

- I In the Model Builder window, right-click Geometry I and choose Extrude.
- 2 In the Settings window for Extrude, locate the Distances section.

**3** In the table, enter the following settings:

#### Distances (m)

- 2 4 6 8 10 12
- 4 In the Geometry toolbar, click 🟢 Build All.
- **5** Click the 🔁 Wireframe Rendering button in the Graphics toolbar.
- 6 Click the **Zoom Extents** button in the **Graphics** toolbar.

The geometry should correspond to that in Figure 1.

## MATERIALS

Add a material to specify the absorption and scattering coefficients inside the boiler.

Chamber

- I In the Materials toolbar, click 🚦 Blank Material.
- 2 In the Settings window for Material, type Chamber in the Label text field.
- 3 Locate the Material Contents section. In the table, enter the following settings:

Property	Variable	Value	Unit	Property group
Absorption coefficient	kappaR	absC(z)	l/m	Basic
Scattering coefficient	sigmaS	scattC	l/m	Basic

Analogously, specify the emissivity of the boiler walls using a material.

#### Walls

- I In the Materials toolbar, click 🚦 Blank Material.
- 2 In the Settings window for Material, type Walls in the Label text field.

- **3** Locate the **Geometric Entity Selection** section. From the **Geometric entity level** list, choose **Boundary**.
- 4 From the Selection list, choose All boundaries.
- 5 Locate the Material Contents section. In the table, enter the following settings:

Property	Variable	Value	Unit	Property group
Surface emissivity	epsilon_rad	em	I	Basic

#### RADIATION IN PARTICIPATING MEDIA (RPM)

- I In the Model Builder window, under Component I (compl) click Radiation in Participating Media (rpm).
- **2** In the Settings window for Radiation in Participating Media, locate the Participating Media Settings section.
- 3 Find the Radiation settings subsection. From the  $P_{\text{index}}$  list, choose 1.

By default, the **Discrete ordinates method** is **S4**, which corresponds to 24 discrete angular directions. To obtain the maximum resolution of 80 directions, select **S8** from the list. Note, however, that this requires approximately 20 GB of memory.

Participating Medium 1

- In the Model Builder window, under Component I (compl)>
  Radiation in Participating Media (rpm) click Participating Medium I.
- 2 In the Settings window for Participating Medium, locate the Model Input section.
- **3** In the *T* text field, type T(z).

#### Initial Values 1

- I In the Model Builder window, click Initial Values I.
- 2 In the Settings window for Initial Values, locate the Initial Values section.
- **3** In the  $T_{\text{init}}$  text field, type T(z).

#### Opaque Surface I

- I In the Model Builder window, click Opaque Surface I.
- 2 In the Settings window for Opaque Surface, locate the Model Input section.
- **3** In the *T* text field, type Tlow.

# **Opaque Surface 2**

I In the Physics toolbar, click 📄 Boundaries and choose Opaque Surface.

2 Select Boundaries 82, 84, 86, 88, 90, and 92 only.

For more convenience in selecting these boundaries, you can click the **Paste Selection** button and paste the above numbers.

- 3 In the Settings window for Opaque Surface, locate the Model Input section.
- **4** In the *T* text field, type Thot.
- 5 Locate the Surface Radiative Properties section. From the Surface type list, choose Black surface.

**Opaque Surface 3** 

- I In the Physics toolbar, click 🔚 Boundaries and choose Opaque Surface.
- **2** Select Boundaries 12, 19, 26, 33, and 40 only.
- 3 In the Settings window for Opaque Surface, locate the Model Input section.
- **4** In the *T* text field, type Tlow.

#### MESH I

Mapped I

- I In the Mesh toolbar, click  $\bigwedge$  More Generators and choose Mapped.
- 2 Select Boundary 5 only.
- 3 In the Settings window for Mapped, click 📗 Build Selected.

Free Quad I

- I In the Mesh toolbar, click  $\bigwedge$  More Generators and choose Free Quad.
- **2** Select Boundary 2 only.

3 In the Settings window for Free Quad, click 📗 Build Selected.

Swept 1

In the **Mesh** toolbar, click As Swept.

#### Size

- I In the Model Builder window, click Size.
- 2 In the Settings window for Size, locate the Element Size section.
- 3 From the Predefined list, choose Extra fine.
- 4 In the Model Builder window, right-click Mesh I and choose Build All.

#### STUDY I

In the **Home** toolbar, click **= Compute**.

#### RESULTS

#### Incident Radiation (rpm)

The default plot groups show the **Incident Radiation** slice plot and the **Net Radiative Heat Flux** surface plot. Follow the instructions below to replace the multislice plot for **Incident Radiation** by a contour plot.

#### Multislice 1

- I In the Model Builder window, expand the Incident Radiation (rpm) node.
- 2 Right-click Multislice I and choose Delete.
- **3** Click **Yes** to confirm.

#### Incident Radiation (rpm)

In the Model Builder window, under Results click Incident Radiation (rpm).

#### Contour I

- I In the Incident Radiation (rpm) toolbar, click 🛞 Contour.
- 2 In the Settings window for Contour, locate the Levels section.
- 3 From the Entry method list, choose Levels.
- 4 In the Levels text field, type range(0,1e5,21e5).
- 5 Locate the Coloring and Style section. From the Contour type list, choose Filled.
- 6 Click to expand the Quality section. From the Smoothing list, choose None.
- 7 In the Incident Radiation (rpm) toolbar, click 🗿 Plot.
- 8 Click the **Zoom Extents** button in the **Graphics** toolbar to get the results shown in Figure 2.
- 9 Click the YZ Go to YZ View button in the Graphics toolbar to reproduce the results in Figure 3.

#### Outgoing Radiative Heat Flux (rpm)

I In the Home toolbar, click 🚛 Add Plot Group and choose 3D Plot Group.

Now, replace the net radiative heat flux by the outgoing radiative heat flux in the second graph.

- 2 In the Settings window for 3D Plot Group, type Outgoing Radiative Heat Flux (rpm) in the Label text field.
- 3 In the Model Builder window, click Outgoing Radiative Heat Flux (rpm).

# Contour I

I In the Outgoing Radiative Heat Flux (rpm) toolbar, click 🔊 Contour.

- In the Settings window for Contour, click Replace Expression in the upper-right corner of the Expression section. From the menu, choose Component I (compl)>
  Radiation in Participating Media>Boundary fluxes>rpm.qr\_out Outgoing radiative heat flux W/m<sup>2</sup>.
- **3** Locate the **Coloring and Style** section. From the **Contour type** list, choose **Filled**.
- 4 Locate the Quality section. From the Smoothing list, choose None.

Outgoing Radiative Heat Flux (rpm)

Click the **Go to Default View** button in the **Graphics** toolbar to obtain Figure 4.