

COMSOL  
CONFERENCE  
2017 ROTTERDAM

OCTOBER 18-20  
POSTILLION CONVENTION CENTRE  
WTC ROTTERDAM



# Exergy analysis of polymer flooding in clastic reservoirs

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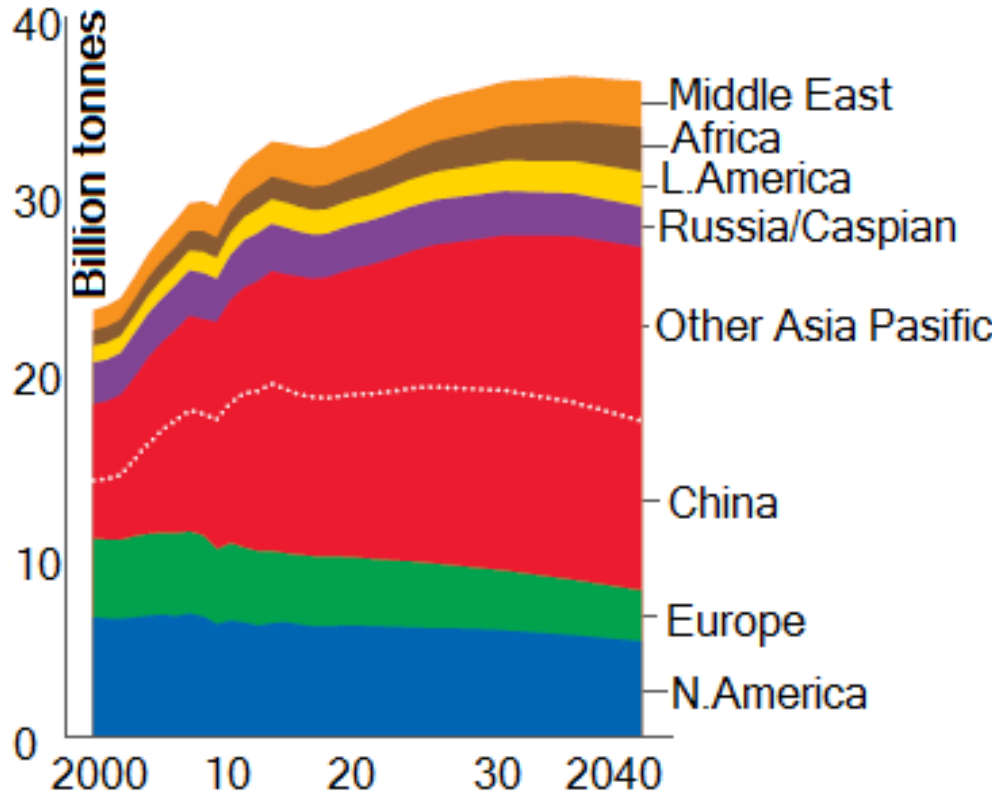
# Agenda – Contents



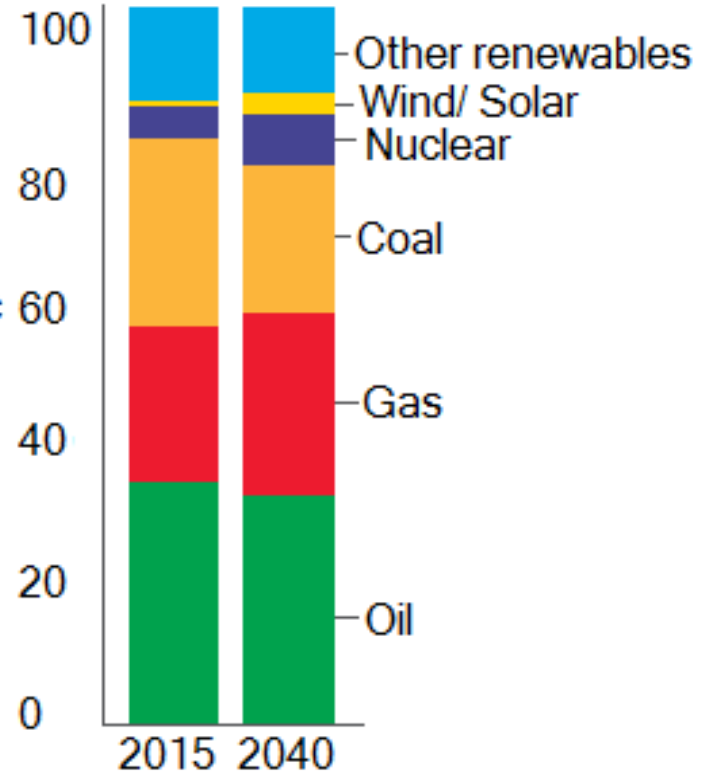
- Introduction
  - Energy outlook (view to 2040)
  - What can be done?
- Objective/ scope of the project
- EOR-polymer flooding
- Why exergy analysis?
- Bio-polymer model(s) results
- Conclusions

# Energy Outlook - view to 2040

## Energy-related CO<sub>2</sub> emissions peak



## Global share of primary energy



(Source: United nation, ExxonMobil estimates, 2017)

# To which extent can the oil and gas industry contribute to this transition (ERoEI)?

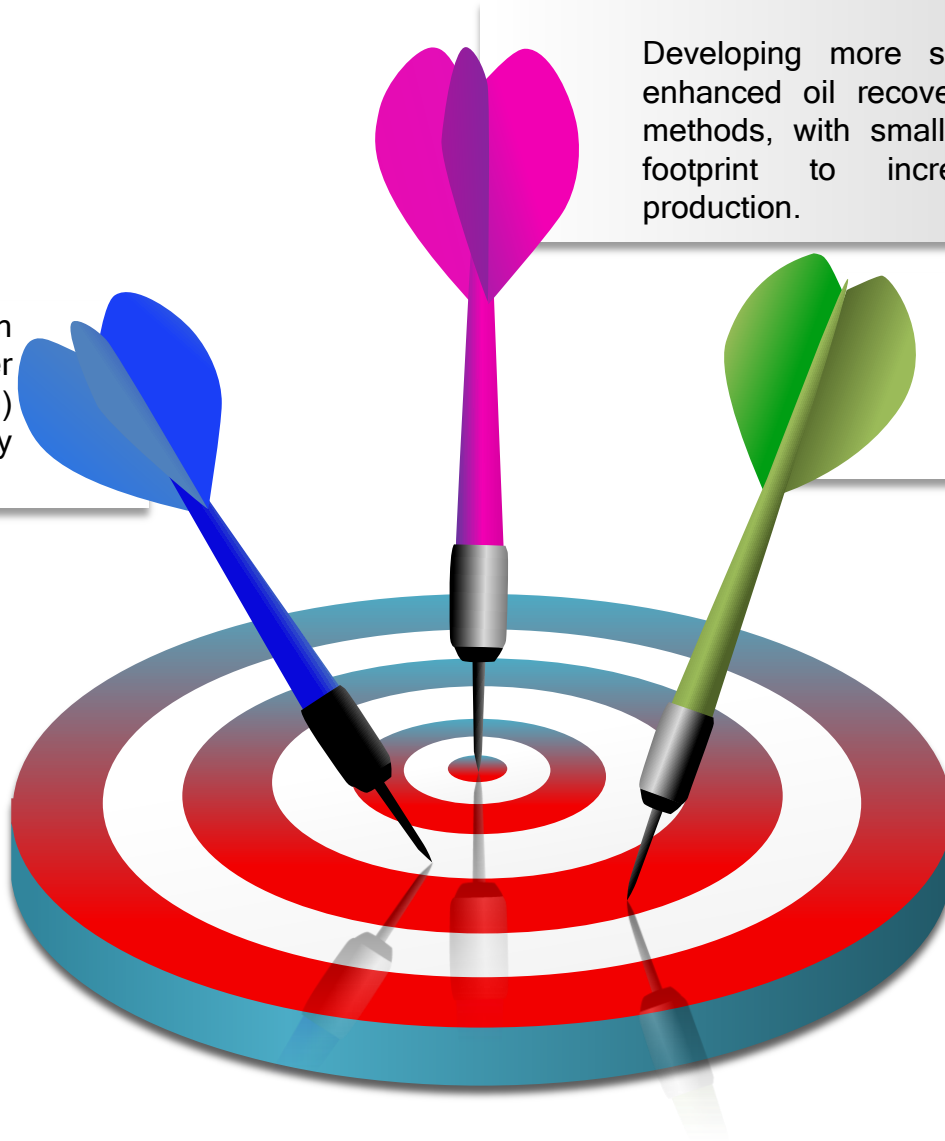
- Exergy can be used to determine whether improved oil recovery is more efficient than conventional oil recovery and therefore reduce the carbon footprint by  $\sim 1\%$
- The possibility to compare energy invested to realize recovery for enhanced and conventional recovery.
- To define marking point (exergy-zero time recovery) when the exergy invested and exergy recovered become the same.

# Objective / scope

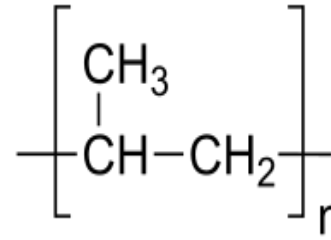
Developing more sustainable enhanced oil recovery (EOR) methods, with smaller carbon footprint to increase oil production.

The focus would be is on injecting natural polymer (Arabic gum / Guar gum) to enhance the recovery behavior.

Analyzing the exergy balance of Arabic gum and showing how such analysis can be done to quantify process efficiency.



# Polymer flooding

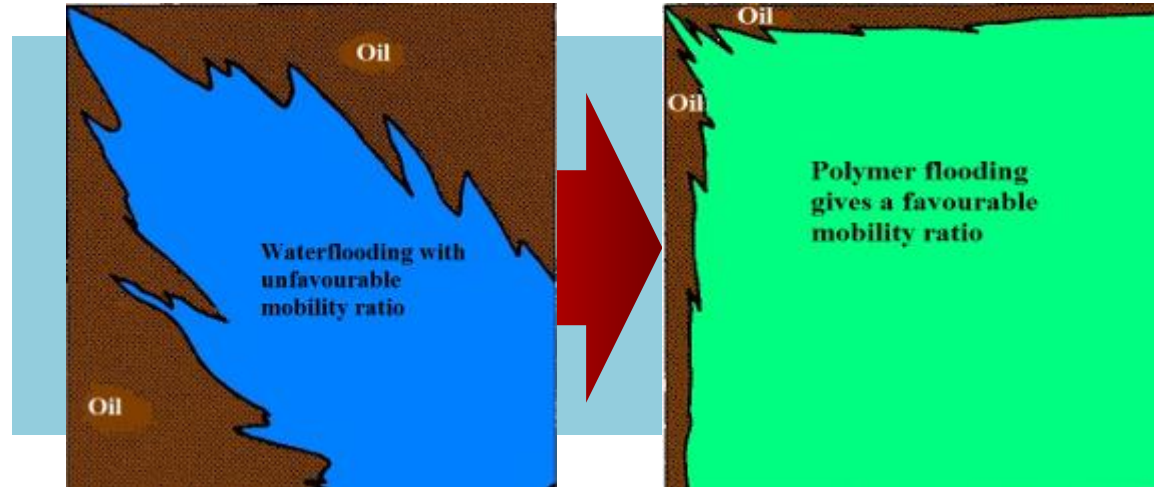


Polymer



Natural  
Arabic gum  
Guar gum

Synthetic  
HPAM  
PAM



$M > 1$   
(Fingering)  
Before Polymer  
Flooding

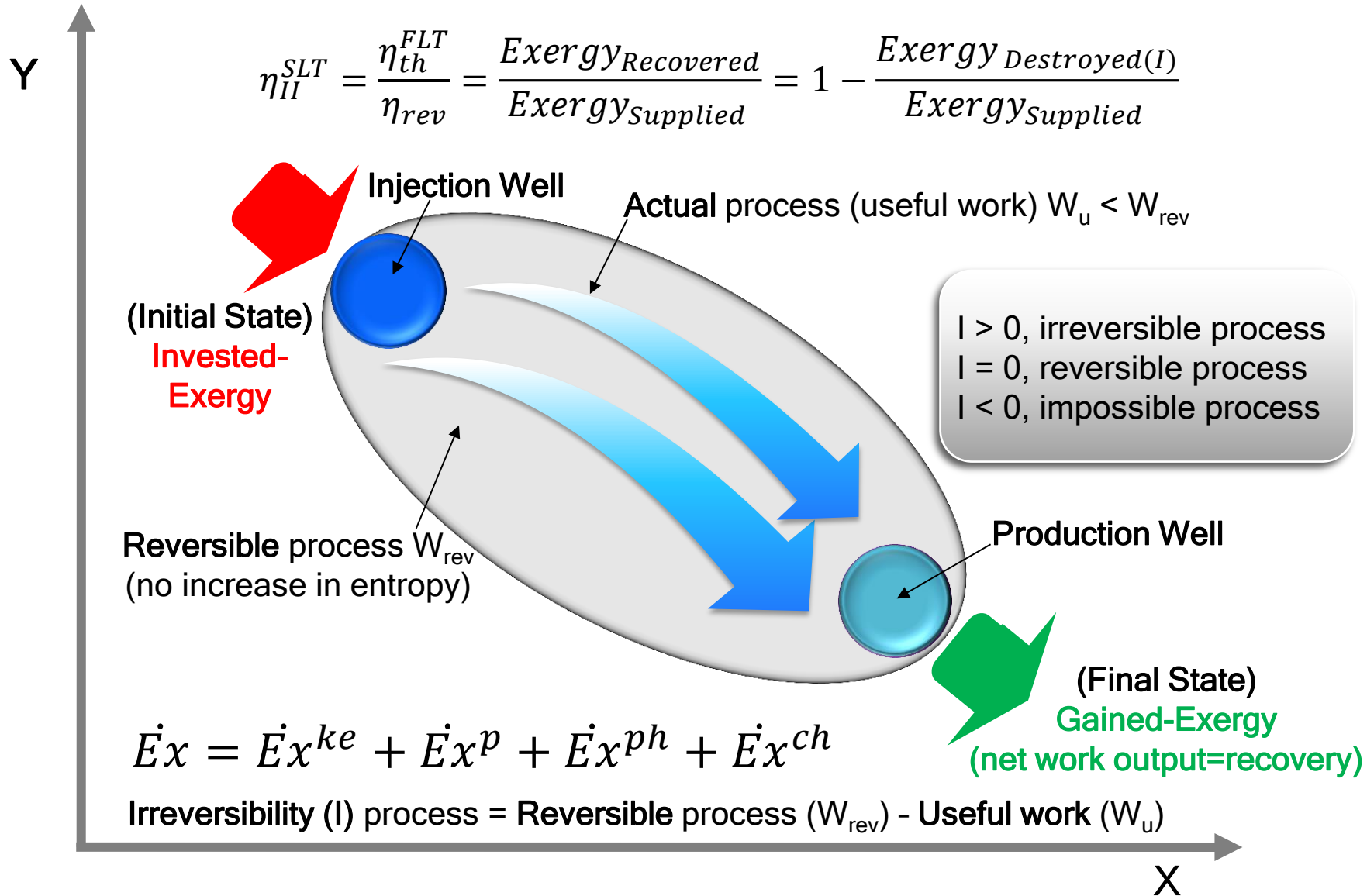
$M < 1$   
(Favorable)  
After Polymer  
Flooding

$$M = \frac{\lambda_{\text{water}}}{\lambda_{\text{oil}}} = \frac{\kappa_{\text{water}} / \mu_{\text{water}}}{\kappa_{\text{oil}} / \mu_{\text{oil}}}$$

## Benefits:

- Enhanced oil recovery up to 30%.
- Decreasing the mobility ratio ( $M$ )
- Sweep efficiency (no fingering).
- Less water required for injection.
- Where:  $\kappa$  = permeability;  $\lambda$  = mobility;  
 $\mu$  = viscosity.

# Exergy Analysis







# Main exergy contributors of PBS

## Drilling exergy

Crushing energy  
116 [MJ/m] (PM)



## Polymer exergy

Manufacturing costs: neglect  
 $c \leq 1200$  [ppm]



## Tubing / Casing

35.8 [GJ/ton-steel]  
(PM)



## Circulation exergy

$3 \times \int_0^{length} dx u_{inj} [m/s] \Delta P [J/m^3]$   
[W/m<sup>2</sup>]  
**Invested-exergy**



≈ 80% of  
Total

## Recovery exergy

$u_{inj} [m/s] \times 10.7 \times 10^3$   
[kWh/m<sup>3</sup> -oil]  $\times (1-f_w) [-] =$   
 $u_{inj} \times 3.85 \times 10^{10} [J/m^3] \times (1-f_w)$   
[W/m<sup>2</sup>]  
**Gained-exergy**



## Labour cost

0.215 [€/kWh] ≈  
59.7 [€/GJ]  
(Mackay, 2008)



# Enhanced Oil Recovery (EOR)

## Scenario 1

### Water Injection

- Water injection during the entire process
  - $c = 0$

## Scenario 2

### Polymer Injection

- Constant natural polymer injection during the entire process
  - $c = c_{\text{bound}} = 0.001$

## Scenario 3

### Slug Injection

- Time dependent slug injection
- $C_{\text{bound}} \times [\text{tanh}(t - \text{tjd1}) - \text{tanh}(t - \text{tjd2})]$  where,  $\text{tanh}(x) = (0.5 + 0.5) \times \text{tanh}(x/\delta)$  where,  $\delta = 0.1$
- $\text{tjd1} = 3 \times 10$  [s] &  $\text{tjd2} = 6 \times 10$  [s]

# COMSOL MODEL- architecture

$$\varphi \partial_t S_w + \partial_x (u_{inj} f_w) = 0$$

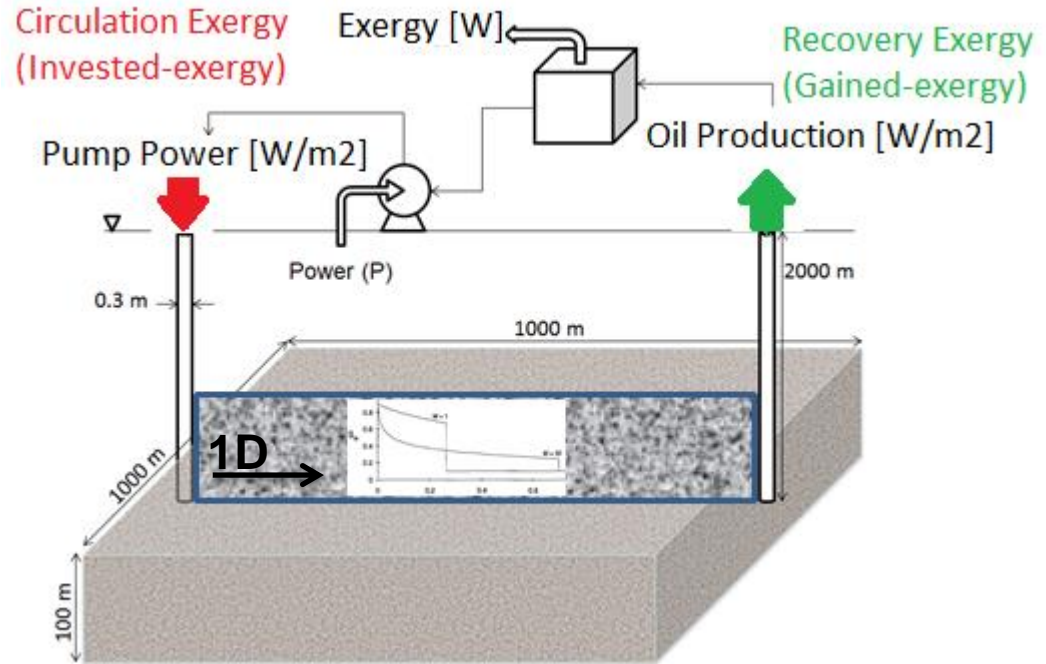
$$\varphi \partial_t (c S_w) + \partial_x (u_{inj} c f_w) = 0$$

where:  $\varphi$  = porosity,  $S_w$  = water saturation,  
 $c$  = polymer-Concentration,  $u_{inj}$  = injection  
 velocity,  $f_w$  = fractional flow function;

$$f_w(S_w, c) = \frac{k_{rw}(S_w) / \mu_w(c; \gamma)}{\frac{k_{rw}(S_w)}{\mu_w(c; \gamma)} + \frac{k_{ro}}{\mu_o}}$$

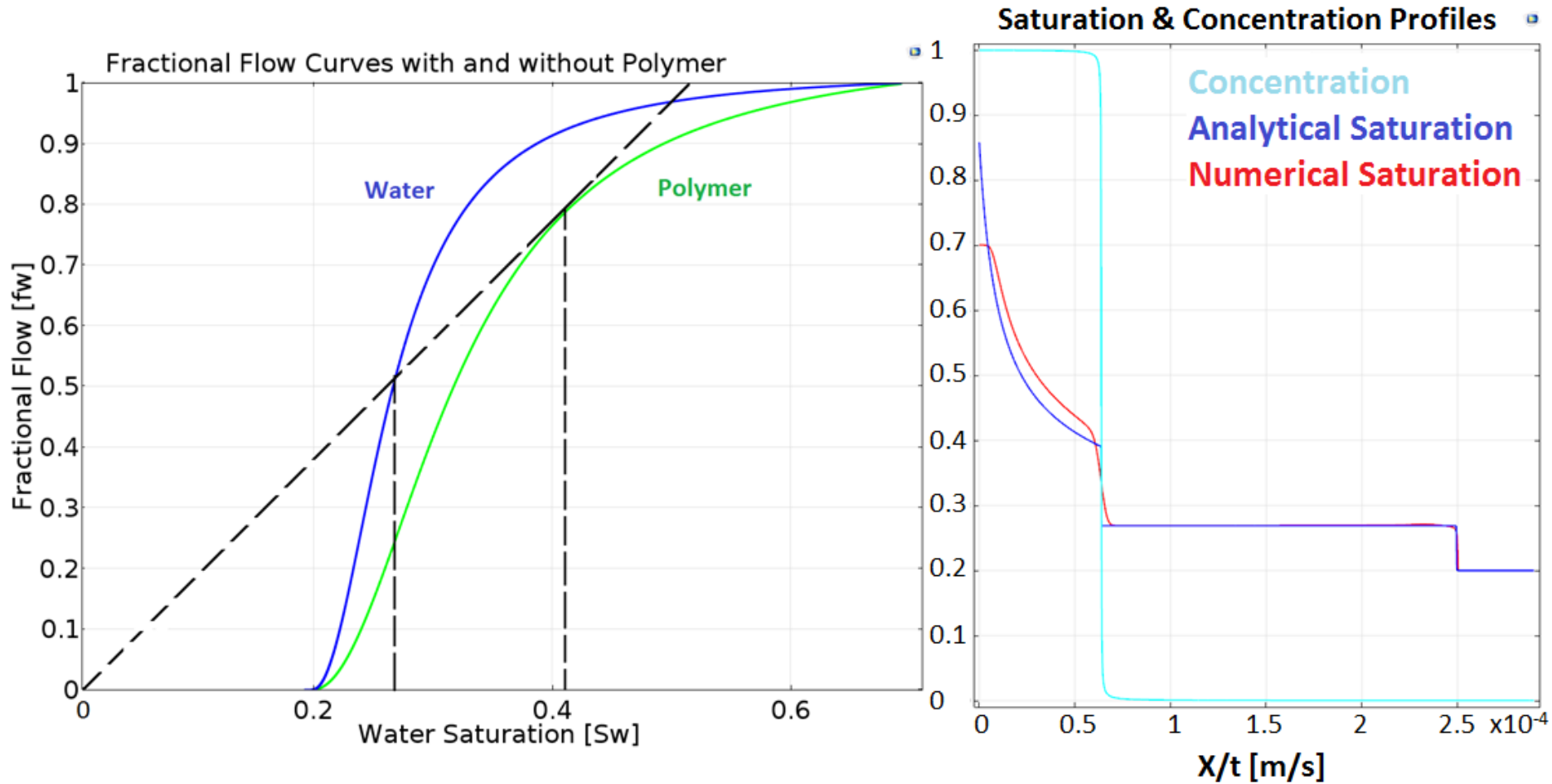
where:  $k_r$  = relative permeability,  $\mu$  = viscosity

Accumulation, Convection, Diffusion

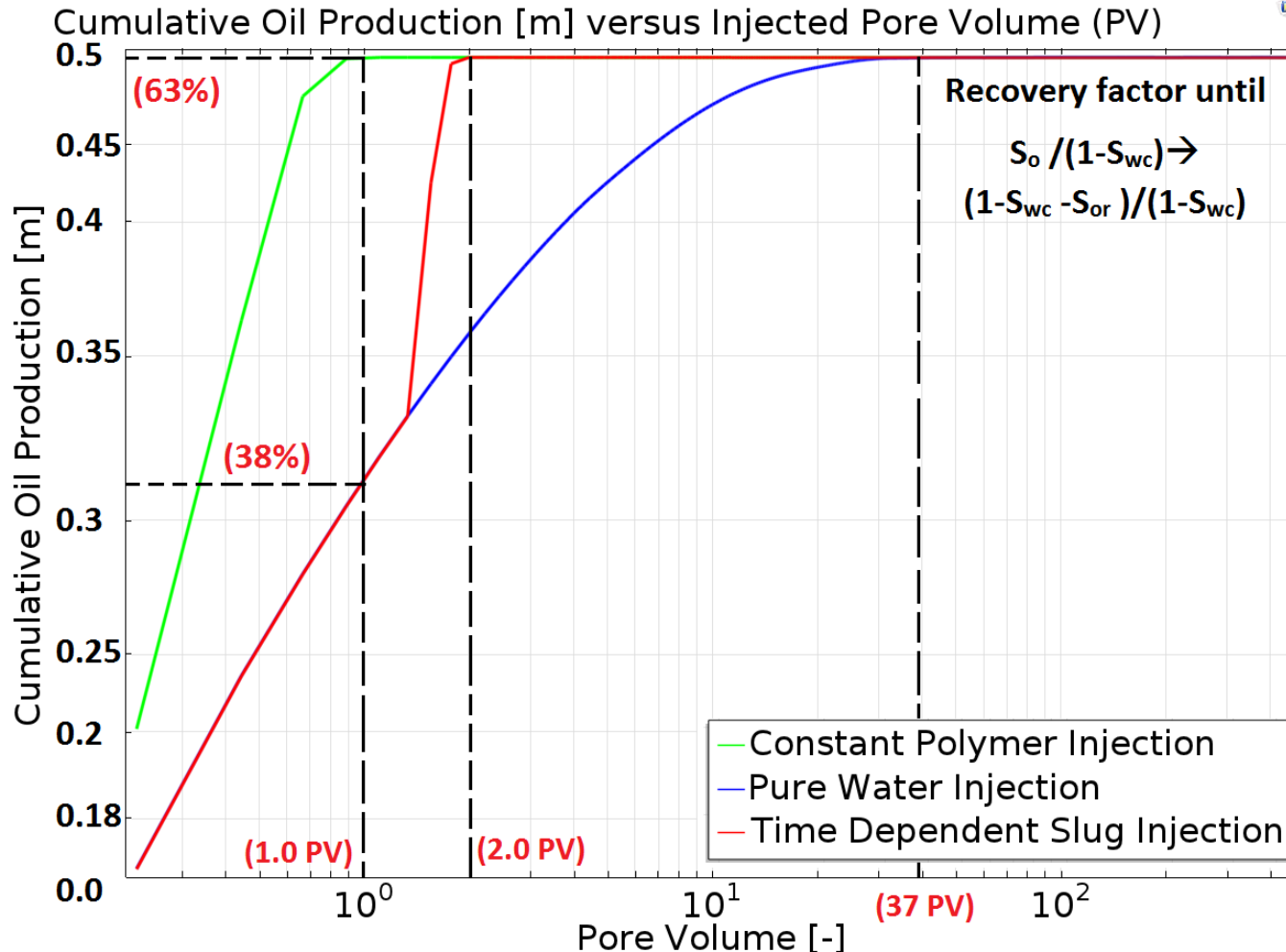


- ❖ **Weak Form1 (Water):**  $\varphi \partial_t(S, t) \times test(S) - u_{inj} \times f_w(S, c) \times test(S_x) + \left(\frac{1}{Pe}\right) \times (S_x) \times test(S_x)$
- ❖ **Weak Form2 (Polymer):**  $\varphi \partial_t(cS, t) \times test(c) - u_{inj} \times c f_w(S, c) \times test(cx) + \left(\frac{1}{Pe}\right) \times (Sc_x) \times test(cx)$

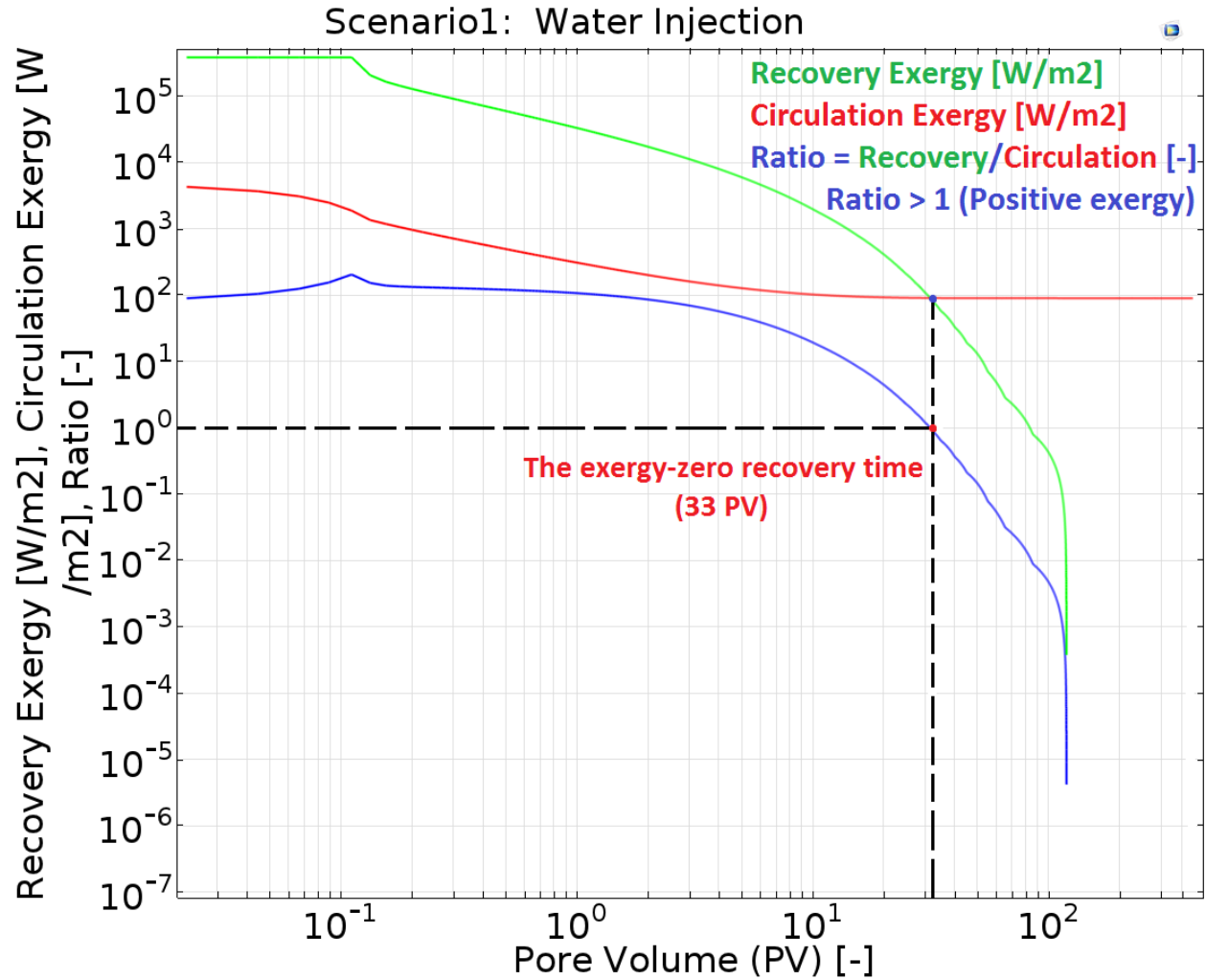
# Results - analytical vs numerical



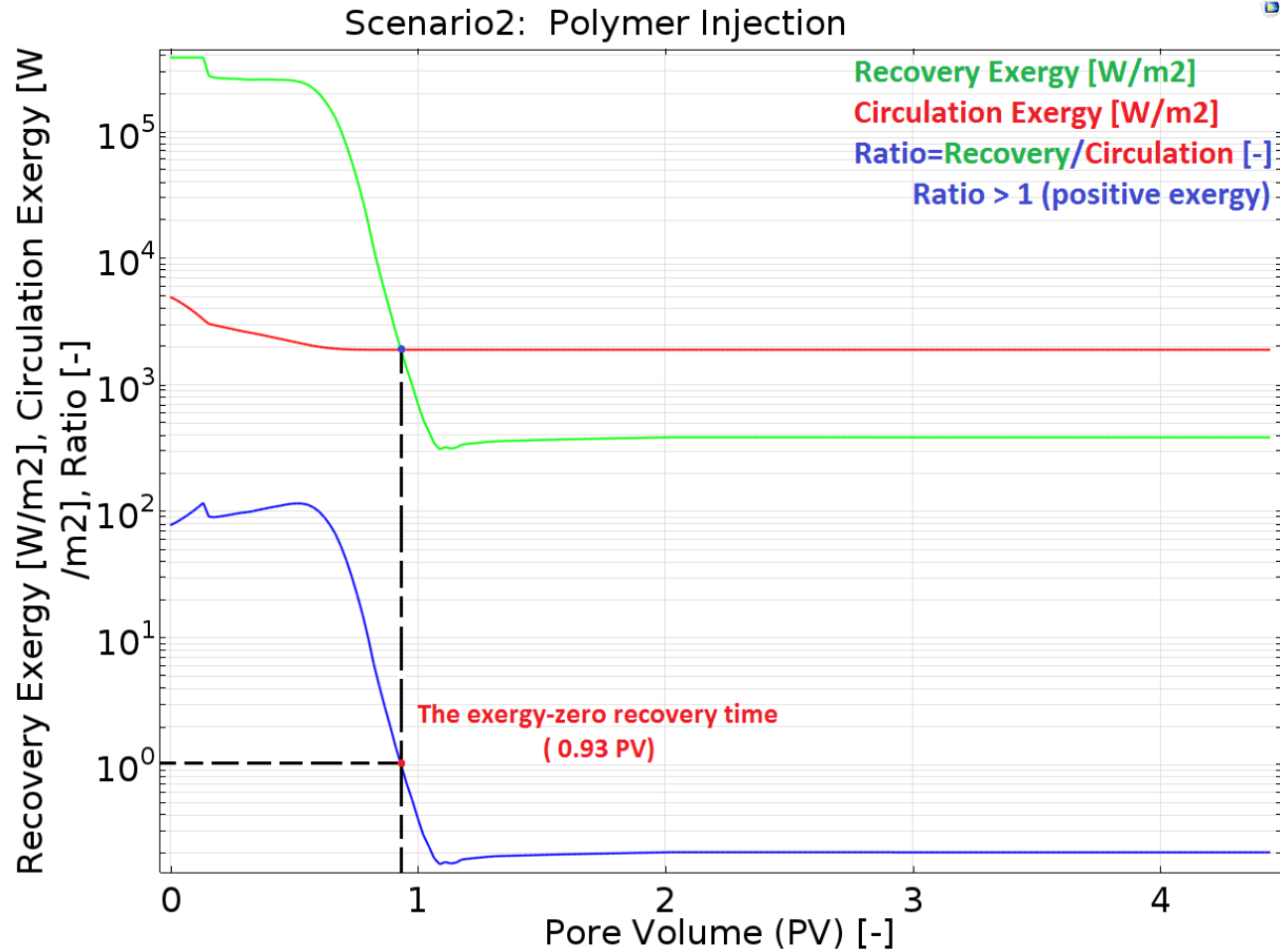
# Results - Recovery Exergy (RF)



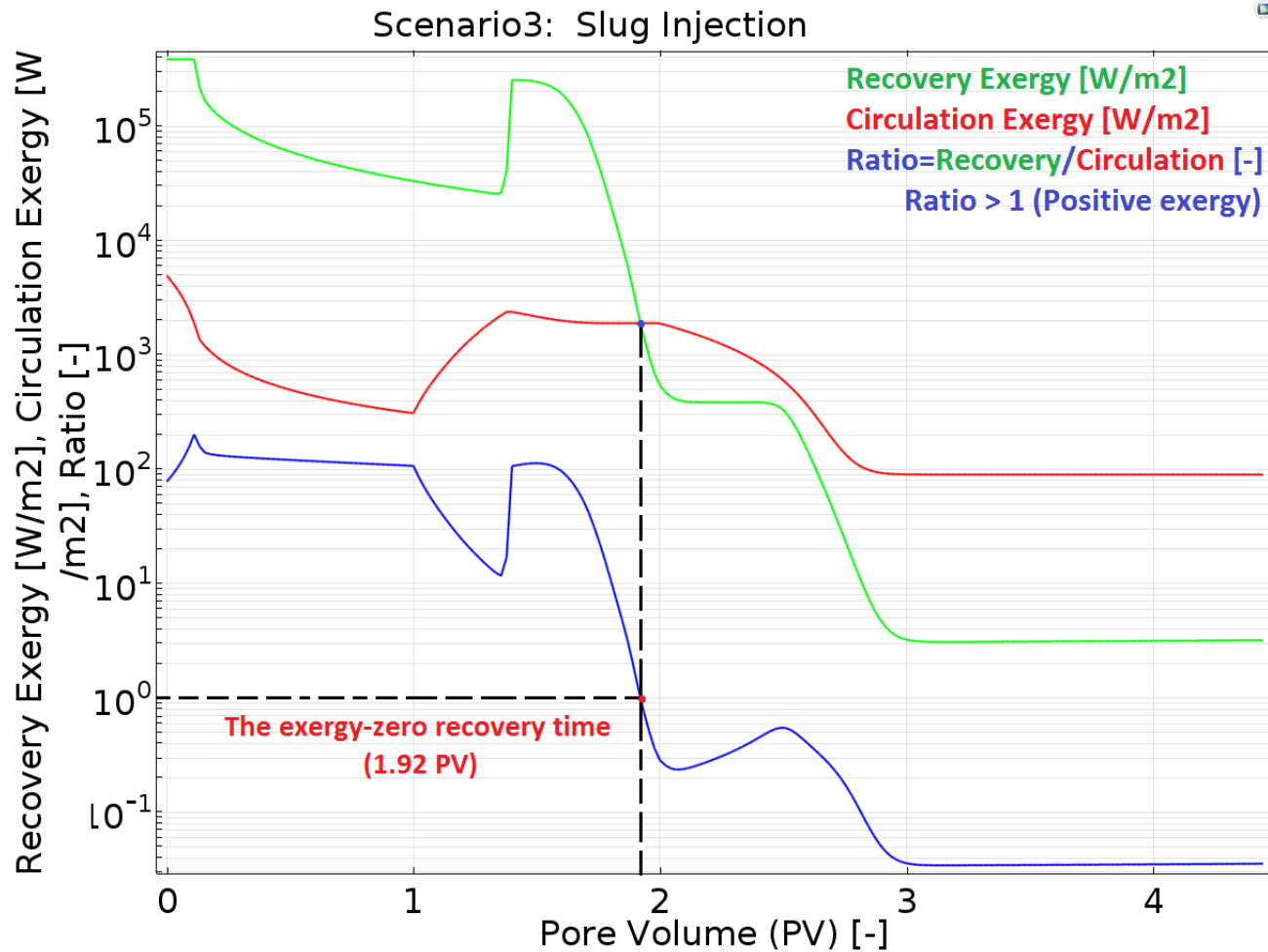
# Results - Scenario 1



# Results - Scenario 2

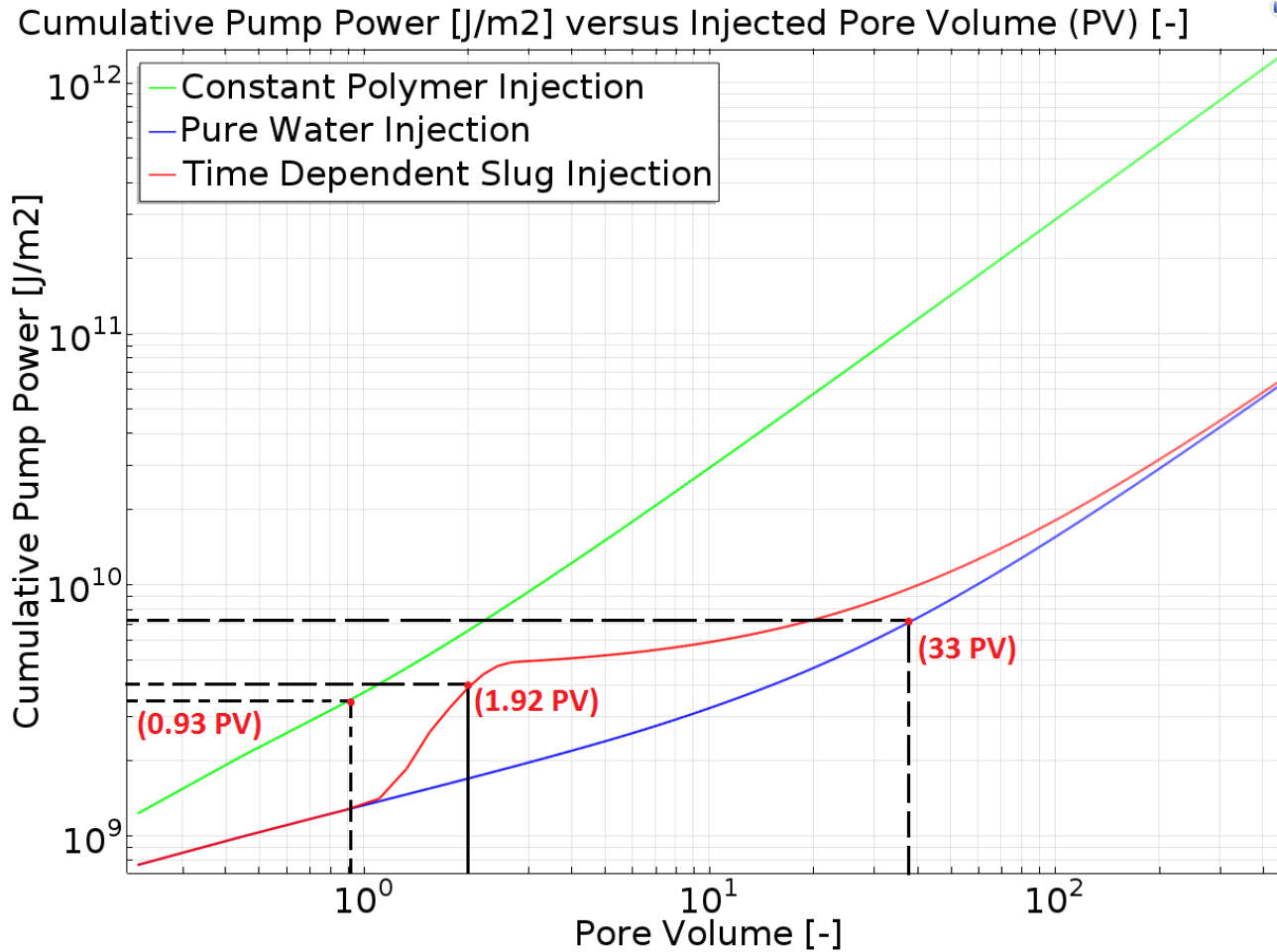


# Results - Scenario 3





# Results - Invested Exergy



# Conclusions

1

Using a 1-D model of polymer displacement it is possible to analyze the exergy (maximum attainable work) balance of viscosified water injection.

2

The circulation exergy is the major contributor, i.e. it exceeds the exergy costs for drilling, casing, tubing and cleaning.

3

The analysis shows that (bio)-polymer injection leads to slightly higher exergy costs for circulation of the fluids, but can for the conditions considered accelerate the production.

4

A consideration for more cases is necessary to decide whether permanent polymer injection can compete with optimized slug injection.

5

The analysis shows that at the end of the project (concept of exergy-zero recovery time), for each scenario the termination point is reached when circulation exergy equal the recovery exergy.



**Questions?**

**Backup slides**

# Energy Outlook - view to 2040

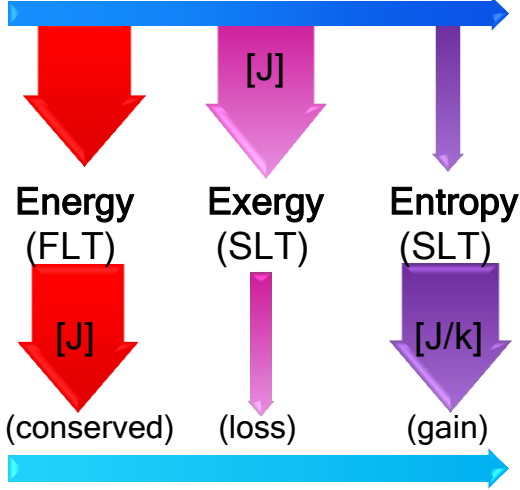
- Modern energy is one of most complex endeavors
- World demographic shift (from 7.3 to **9.1** billion in 2040)
- World economy doubles over the next 20 years (**3.4%**)
  - Global productivity will effectively double (GDP per person)
  - Growth in number of middle class families (2 billion)
  - Emerging economy powers (i.e., China, India)
- Global demand (700 quadrillion BTUs in 2040 ~ **25%**)
- Oil remains the primary fuel ~ **60%** (transport, industry)
- Global CO<sub>2</sub> emissions
  - Global CO<sub>2</sub> emissions rose close to 40% from 2000 to 2015
  - Global CO<sub>2</sub> emissions are likely to **peak** (2015 to 2040)

# Why exergy analysis?

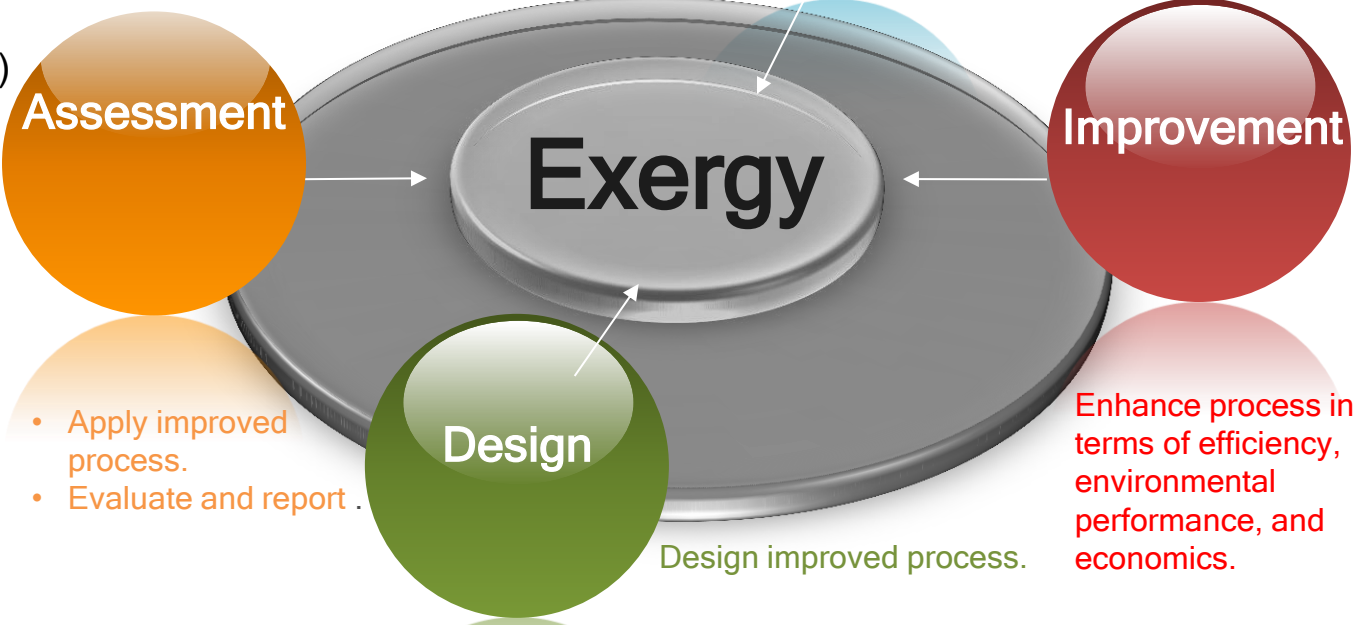
- **Exergy** is a measure of the ability to produce useful work (potential work) from a quantity or flow (i.e. mass, heat) in specific environment (T, P, compositions).
- Energy (quantity) vs. Exergy (quantity & quality): Performing energy/ exergy balances and evaluating process efficiencies.
- Exergy of products = Exergy of resources - Exergy losses

- Combined FLT & SLT
- Measure quantity & quality
- Direction & reversibility aspects.
- Exergy degradation (loss/ irreversibility)

Non-equilibrium State ( $T_1, P_1, x_1$ )  
Exergy of System > 0.

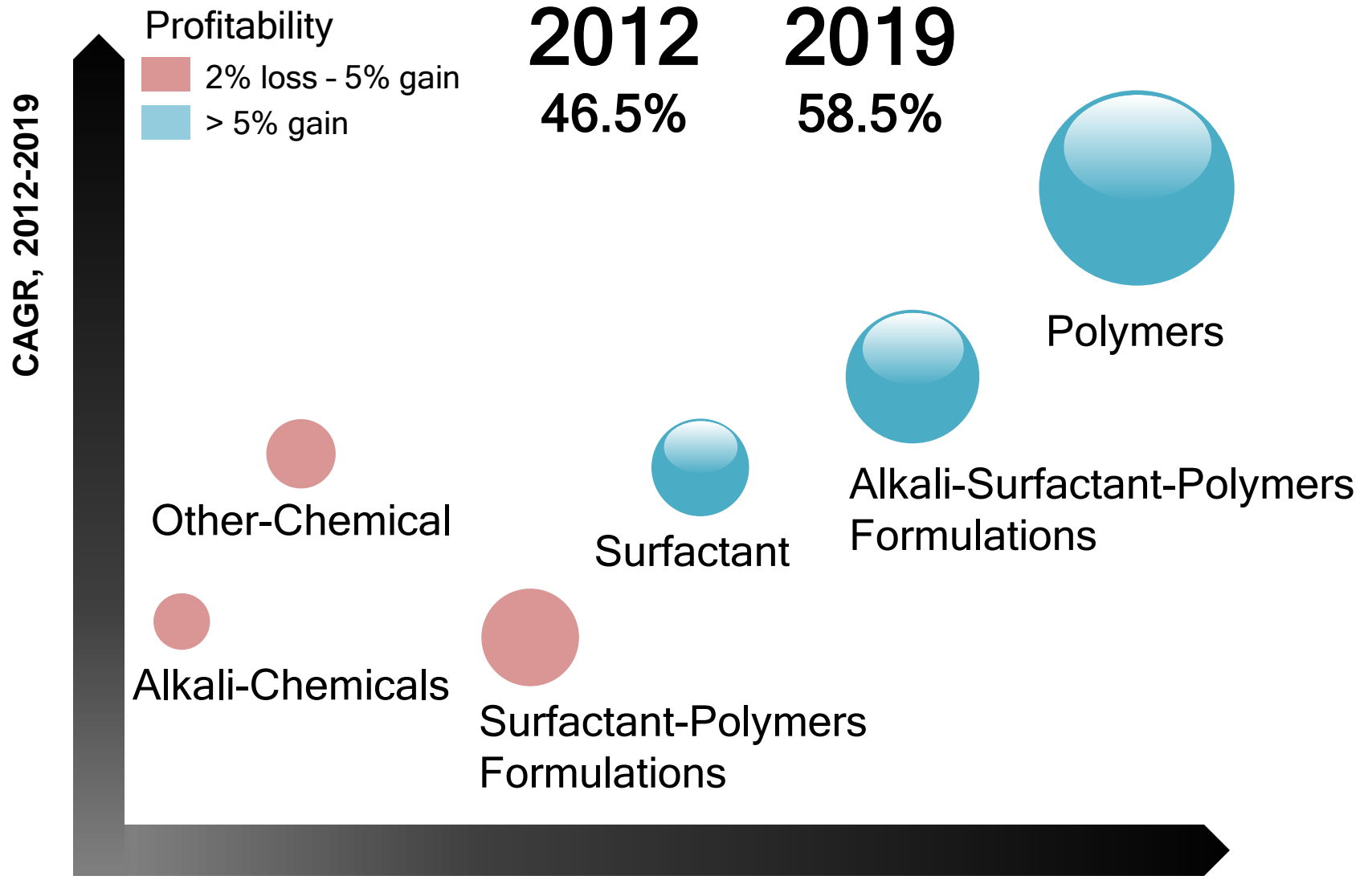


Equilibrium State ( $T_0, P_0, x_0$ ) → (reference environment)  
Exergy of System = 0.



$$\dot{E}x = \dot{E}x^{ke} + \dot{E}x^p + \dot{E}x^{ph} + \dot{E}x^{ch} ; Ex_{RF} = \frac{(Ex_{gained} - Ex_{invested})}{Ex_{gained}}$$

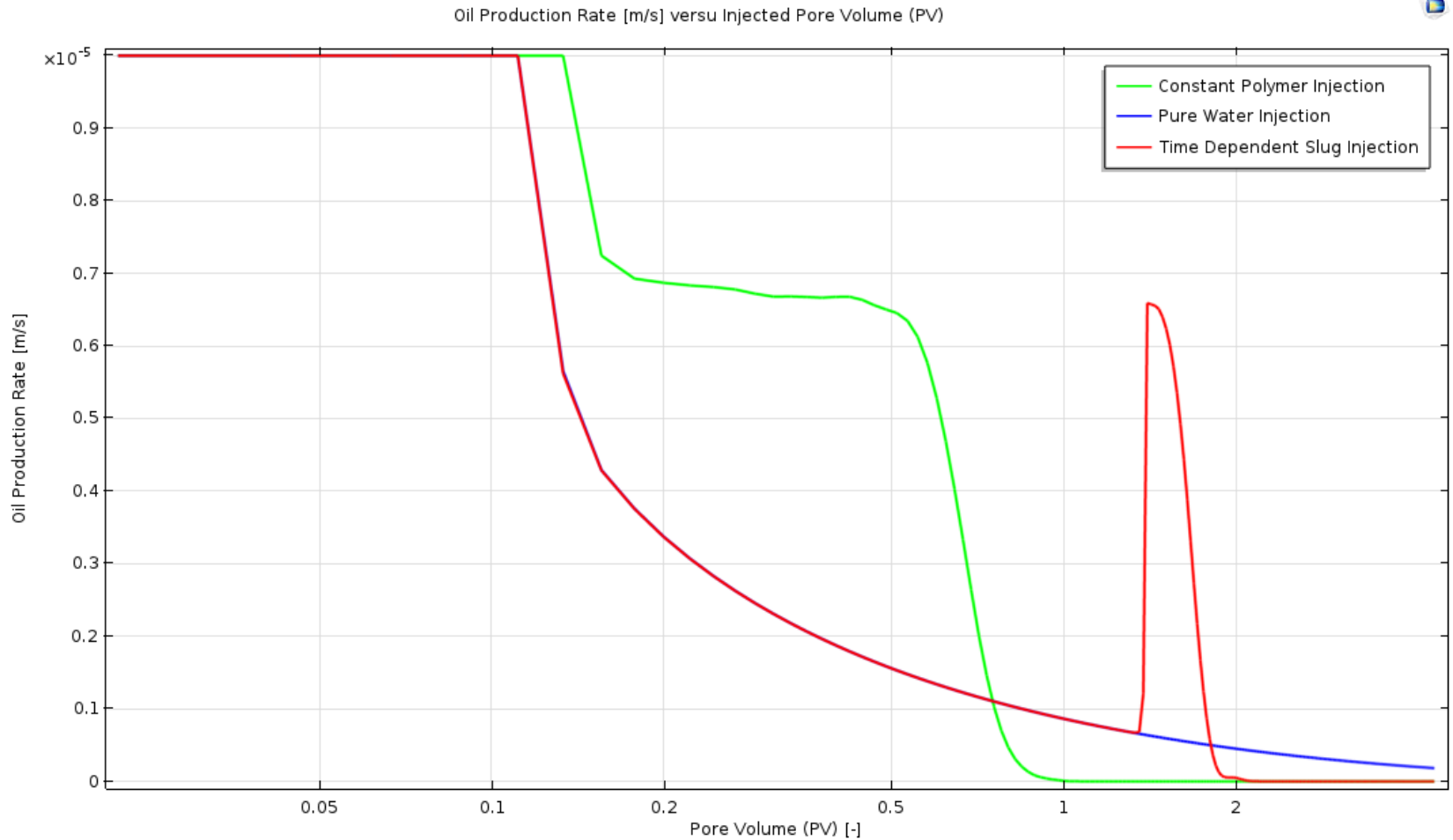
# Growth Opportunities for EOR-polymer Demand



Source: Forst & Sullivan, 2012.

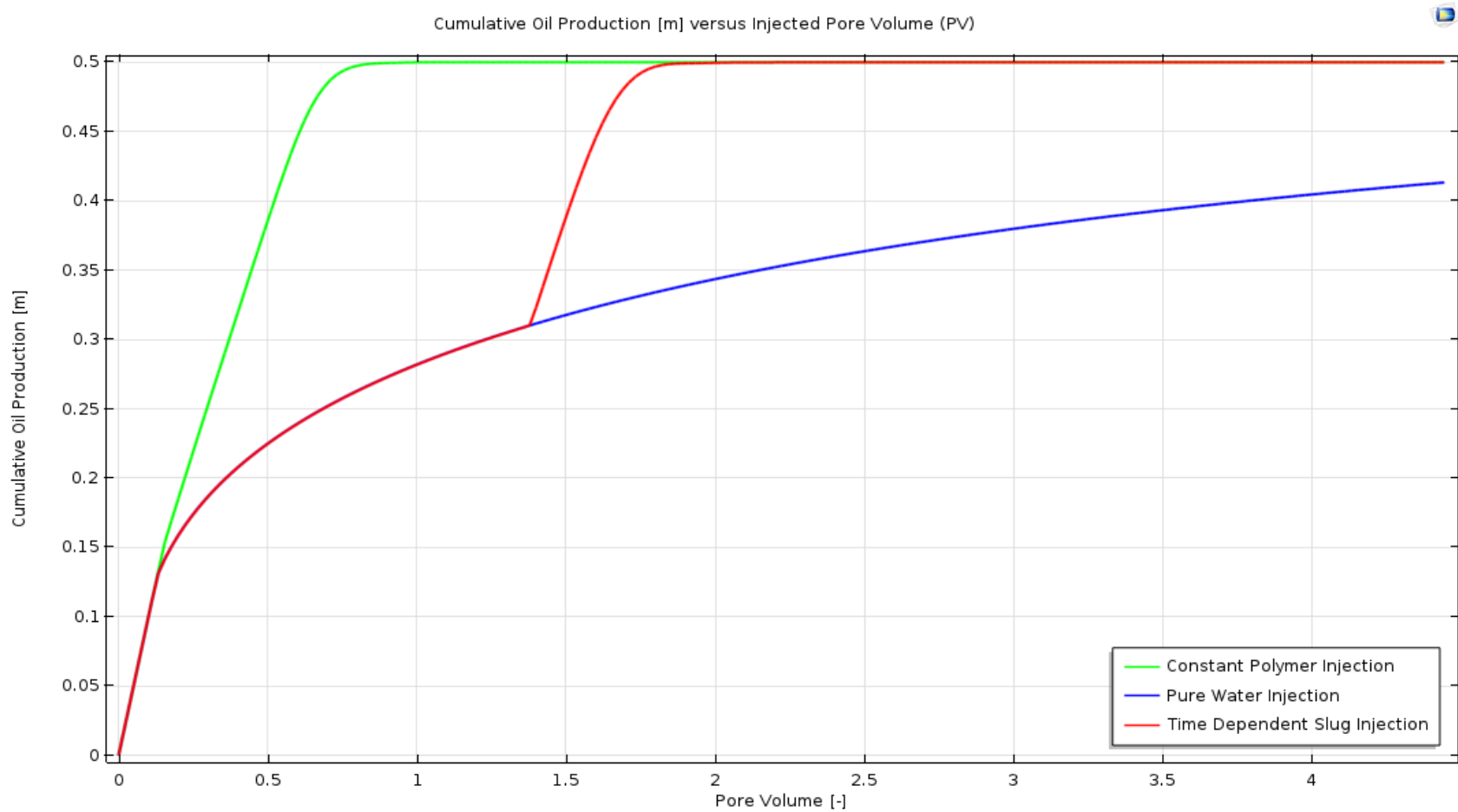
Analysis of Enhanced Oil Recovery Chemical Market in The United States and Europa.

# Results - Oil production rate

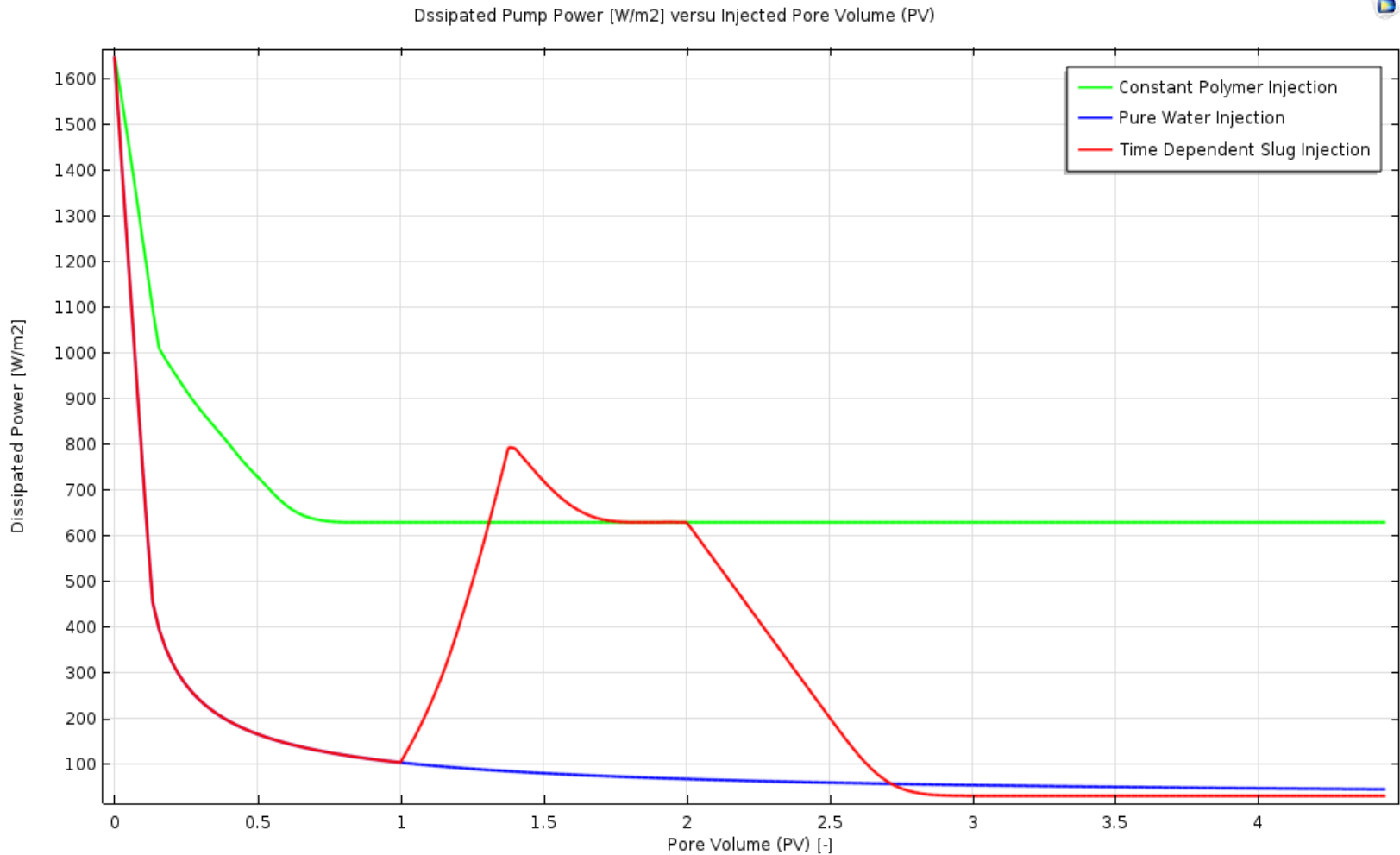




# Results - Cumulative oil production



# Results - Dissipated pump power



# Results - Ratio [-]

Ratio Cumulative Produced Oil [W/m<sup>2</sup>] divided by Dissipated Pump Power [W/m<sup>2</sup>] versus Pore Volume (PV)

