



AACHENER VERFAHRENSTECHNIK

Acid-Base Reactions Enhancing Membrane Separation: Model Development and Implementation

October, 2009

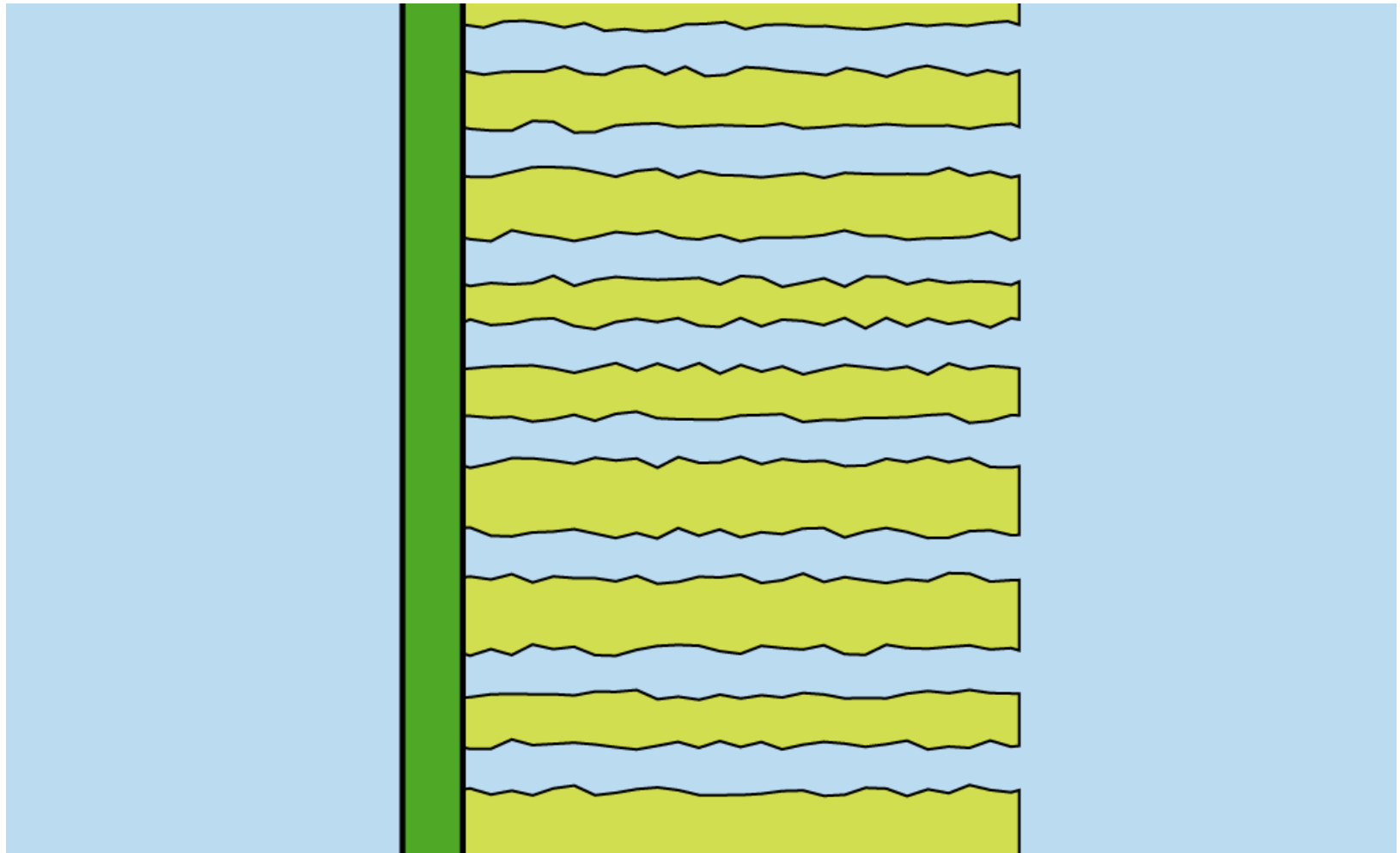
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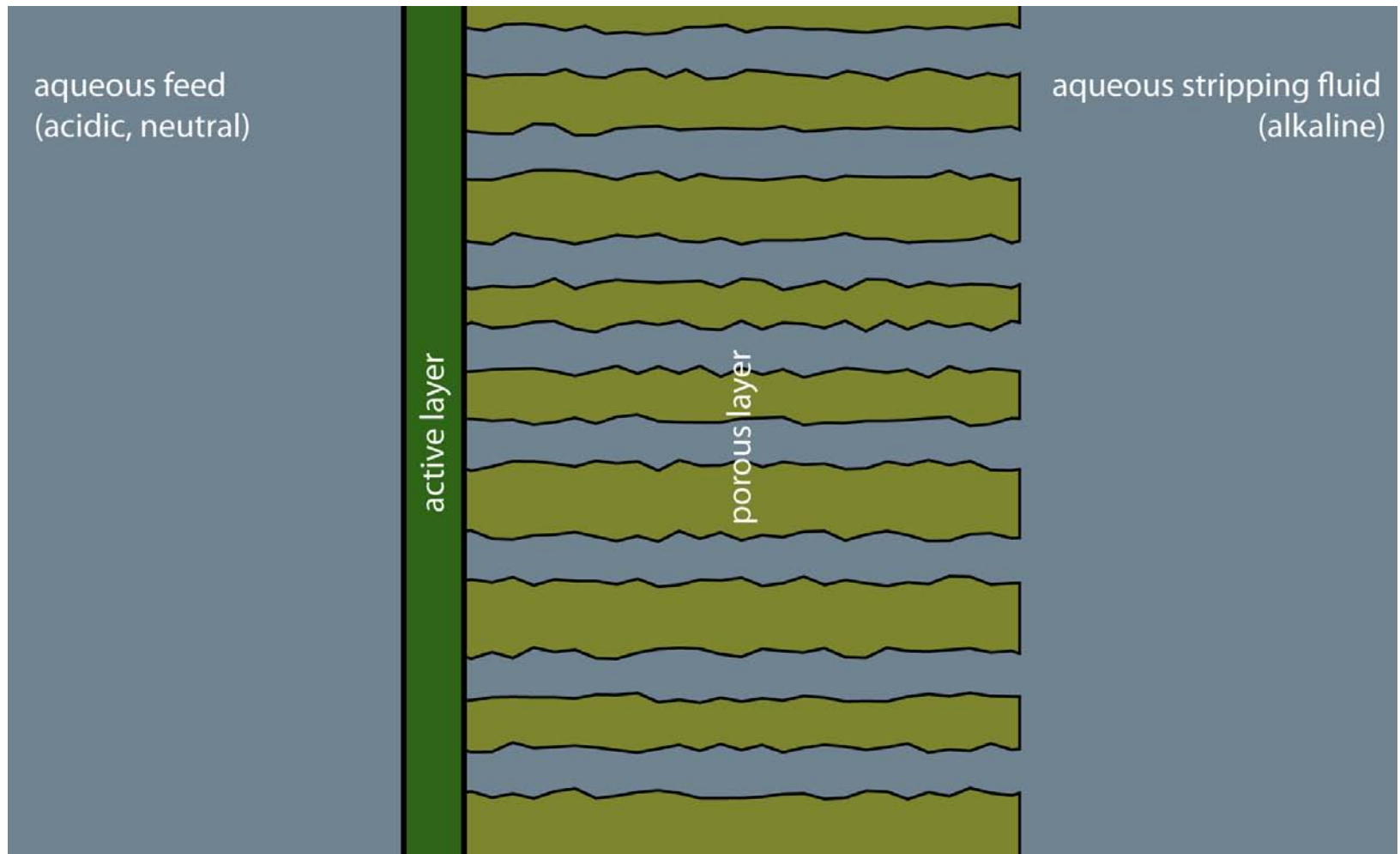
Overview

- Introduction
- Governing Equations
 - Differential-algebraic equations
 - Boundary conditions
 - Implementation
- Verification and Results
 - Alternative Model by Olander
 - Simulation results
- Summary and conclusion

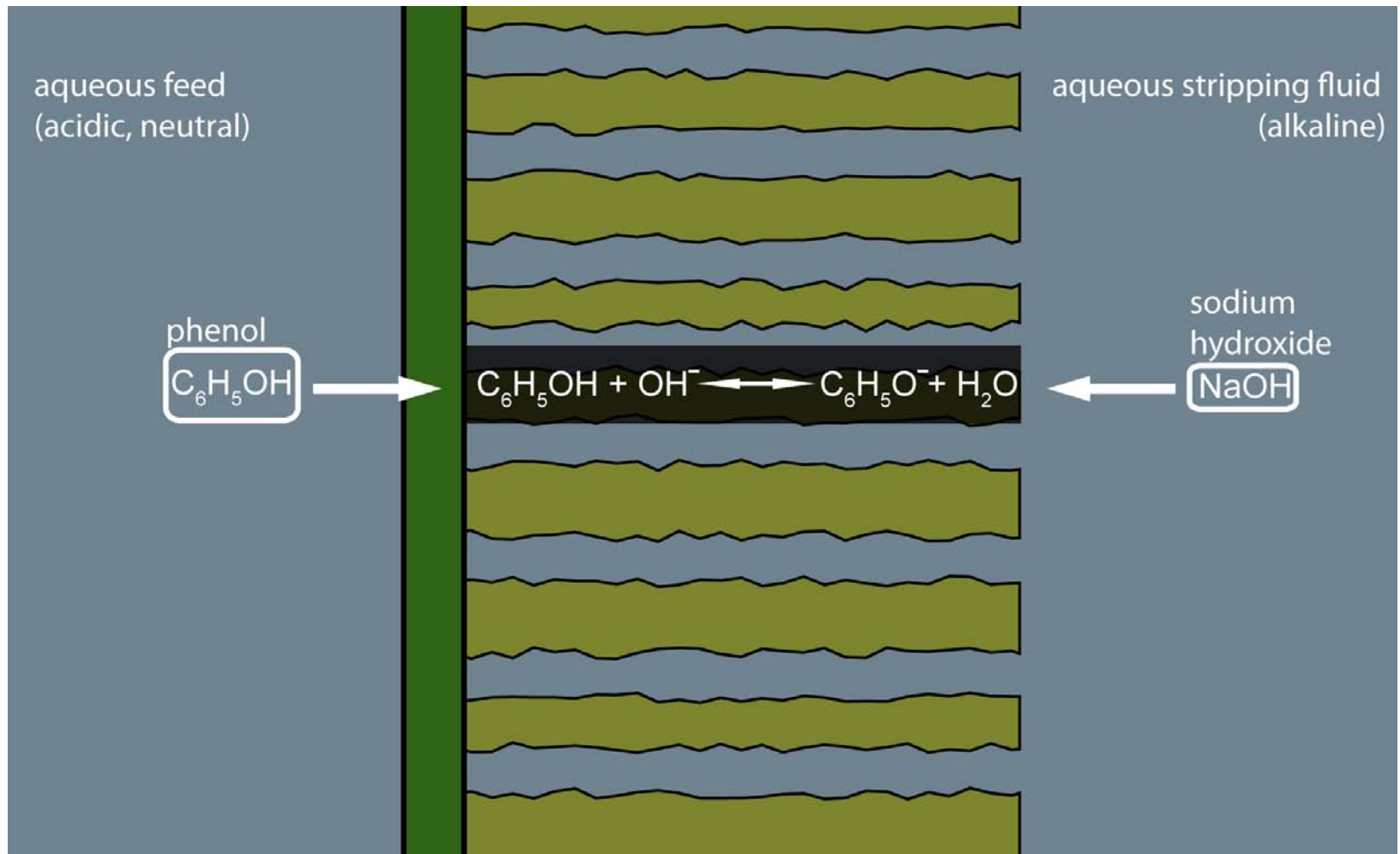
Reactive Extraction of Organic Acids



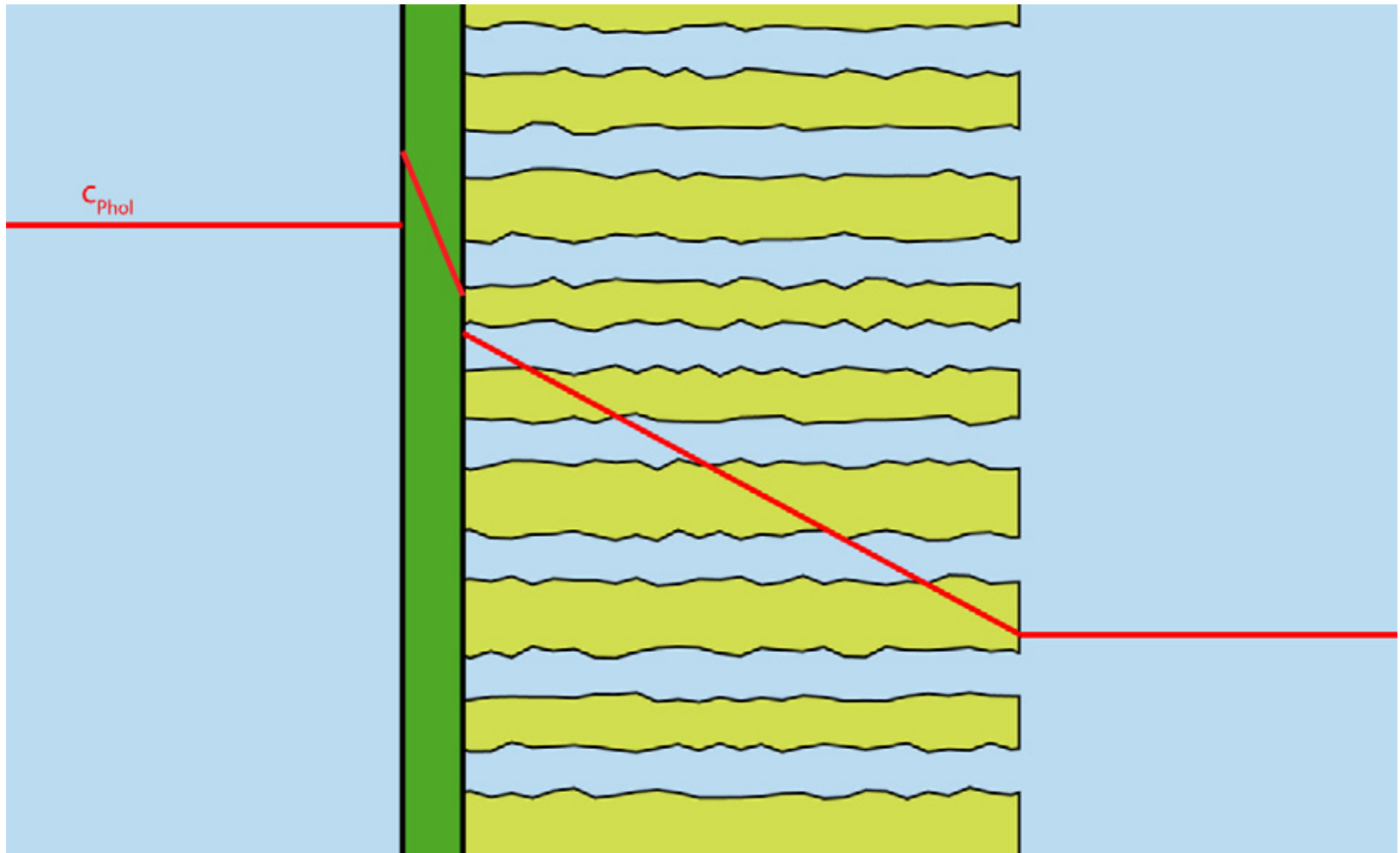
Reactive Extraction of Organic Acids



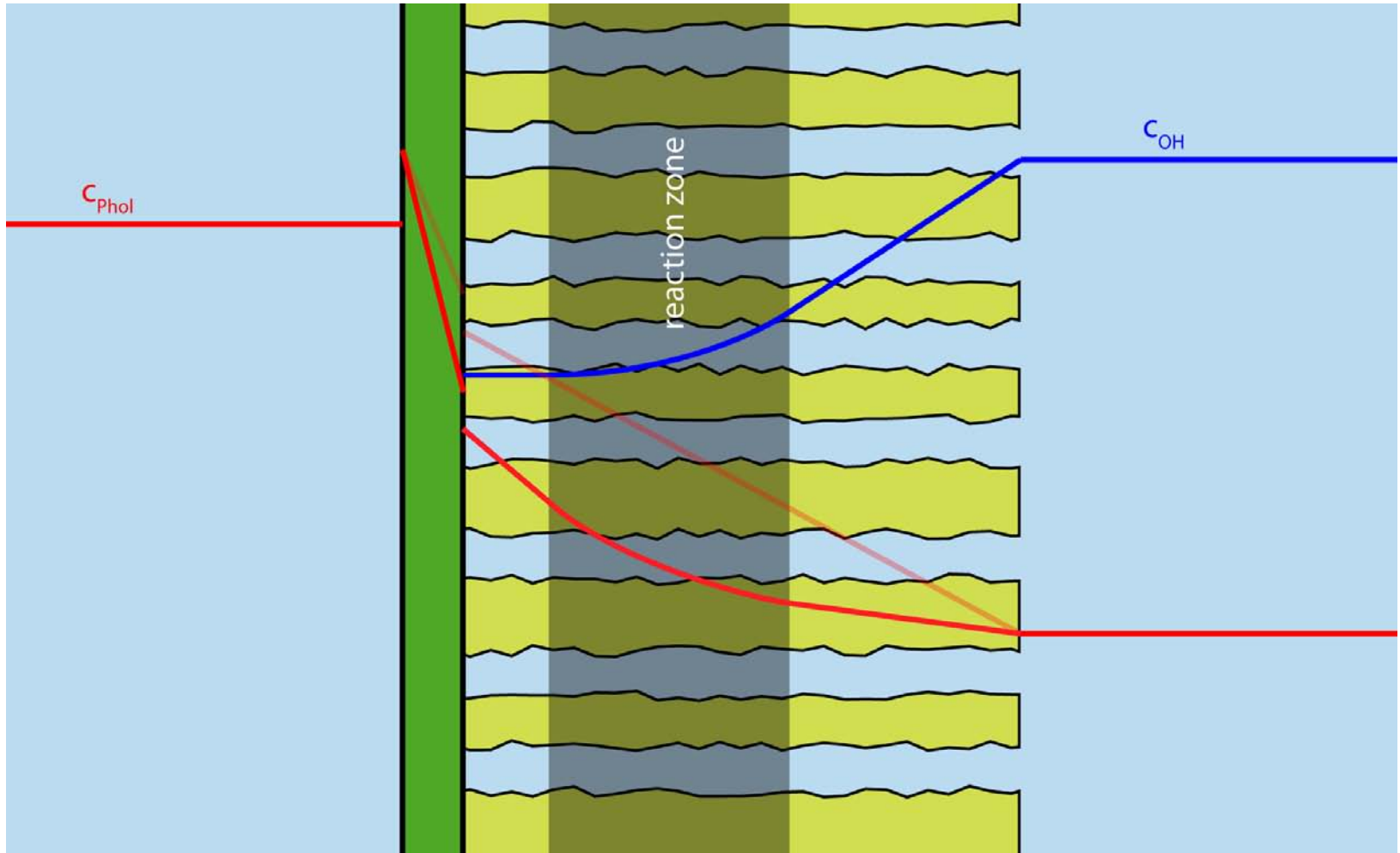
Reactive Extraction of Organic Acids



Reactive Extraction of Organic Acids



Reactive Extraction of Organic Acids



Governing Equations

- Transport equations for phenol, phenolate and OH-Ions

$$(1) \quad 0 = \varepsilon D_{Phol} \frac{\delta^2 c_{Phol}}{\delta Z^2} - R$$

$$(2) \quad 0 = \varepsilon D_{OH} \frac{\delta^2 c_{OH}}{\delta Z^2} - R$$

$$(3) \quad 0 = \varepsilon D_{Phat} \frac{\delta^2 c_{Phat}}{\delta Z^2} + R$$

(1) + (3)

(2) + (3)

$$0 = \varepsilon D_{Phol} \frac{\delta^2 c_{Phol}}{\delta Z^2} + \varepsilon D_{Phat} \frac{\delta^2 c_{Phat}}{\delta Z^2}$$

$$0 = \varepsilon D_{OH} \frac{\delta^2 c_{OH}}{\delta Z^2} + \varepsilon D_{Phat} \frac{\delta^2 c_{Phat}}{\delta Z^2}$$

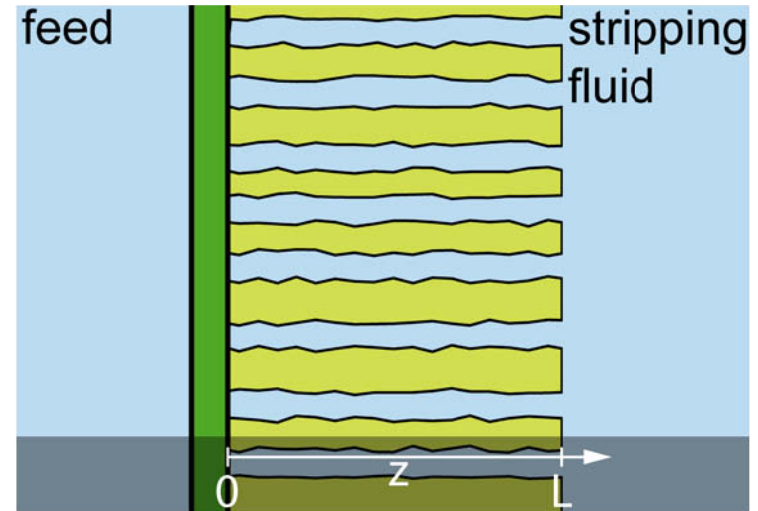
$$R = k_1 c_{Phol} c_{OH} - k_2 c_{Phat}$$

$$K = \frac{k_1}{k_2} = \frac{c_{Phat}}{c_{Phol} \cdot c_{OH}}$$

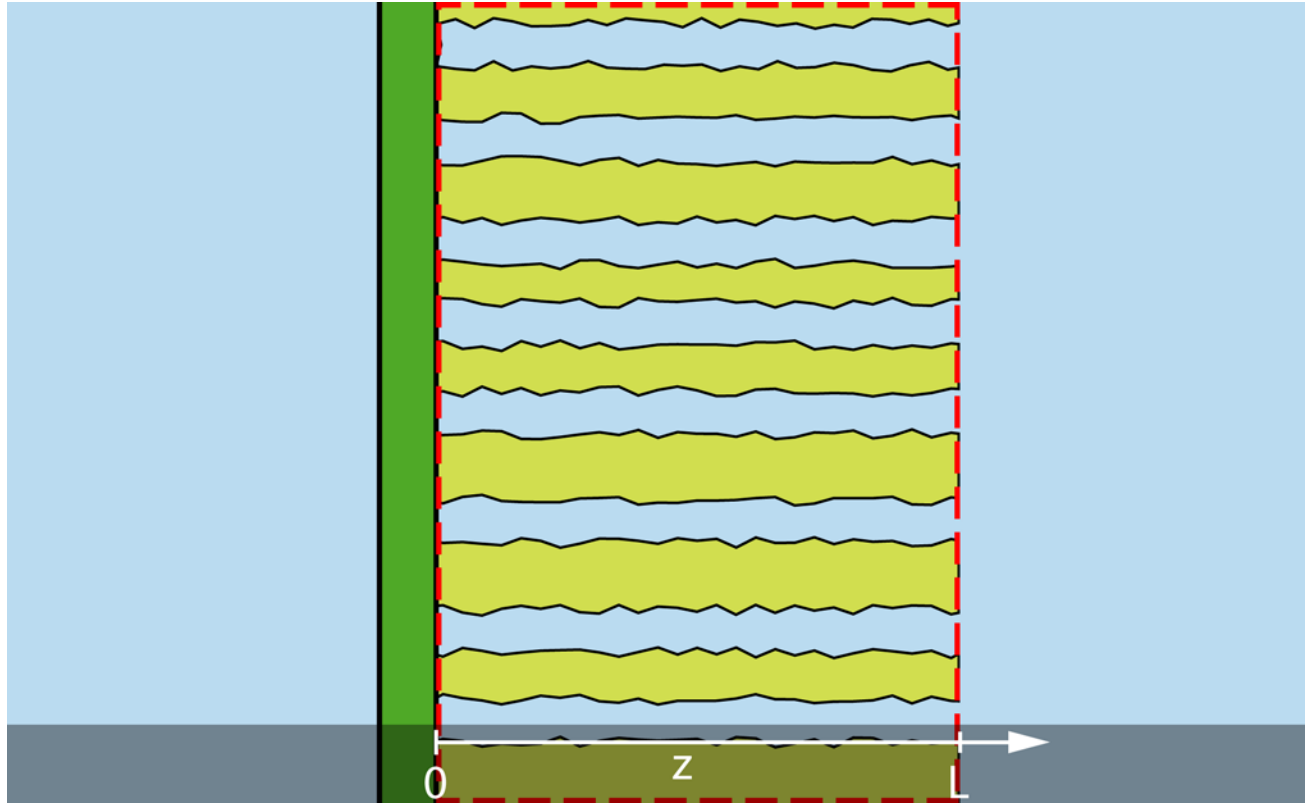
- Problem: Magnitude of Reaction Rate constants k_1 , k_2 undefined
 - Too high: model instabilities
 - Too low: incomplete chemical equilibrium
- Substitution of reaction rates

Boundary Conditions

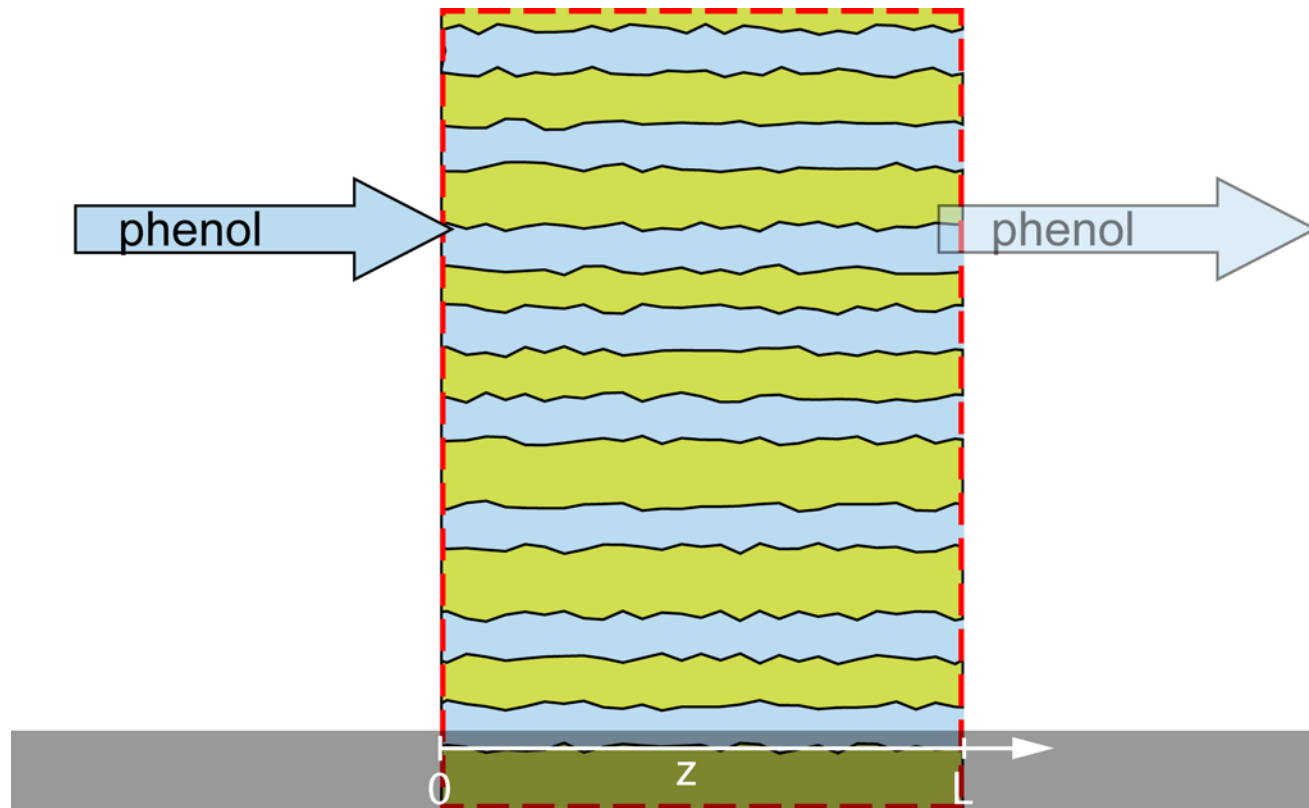
#	Bnd	Species	Condition
1		OH	Insulation
2	z = 0	Phat	Insulation
3		Phol	$\dot{n}_{Phol} = k_{mem} \cdot \Delta c_{Phol}$
4	z = L	Phol	$c_{Phol}^{z=L} = c_{Phol}^{stripp}$
5		Phat	$c_{Phat}^{z=L} = c_{Phat}^{stripp}$



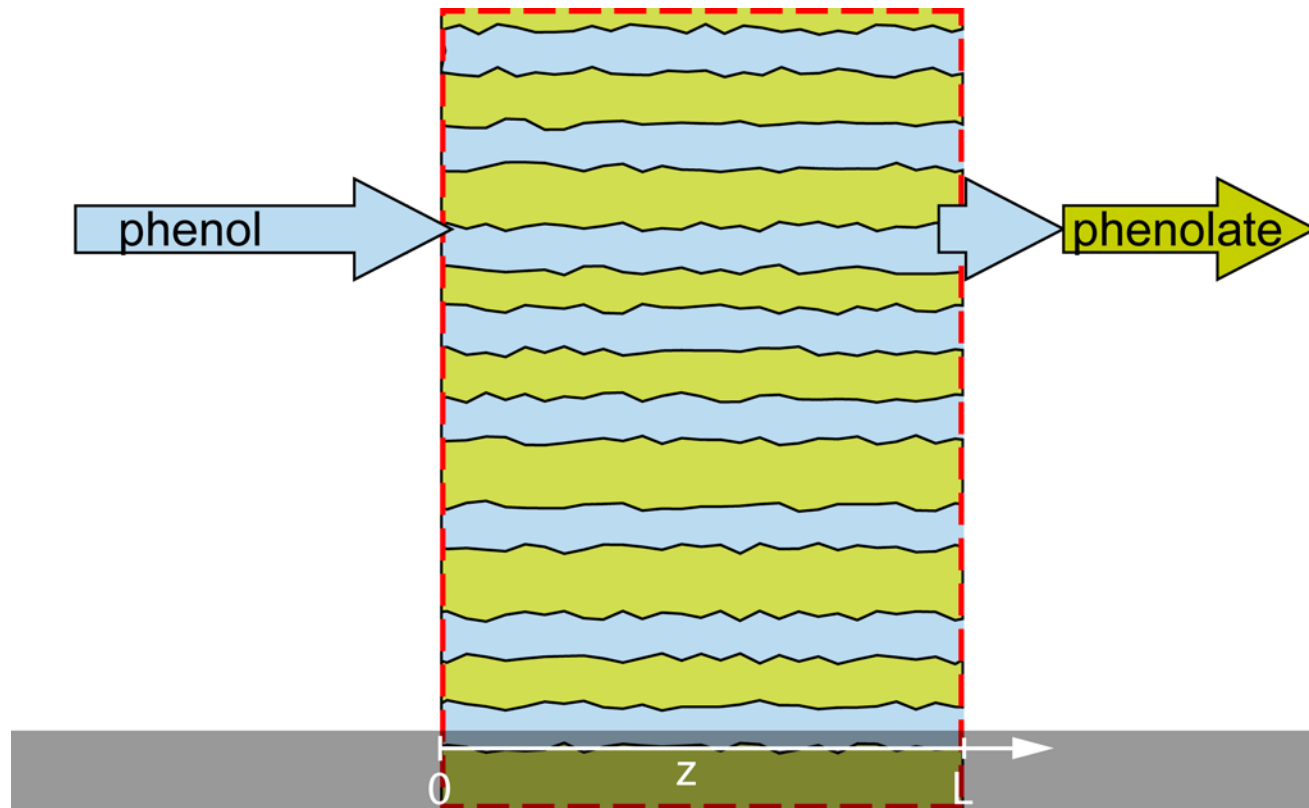
Boundary Conditions



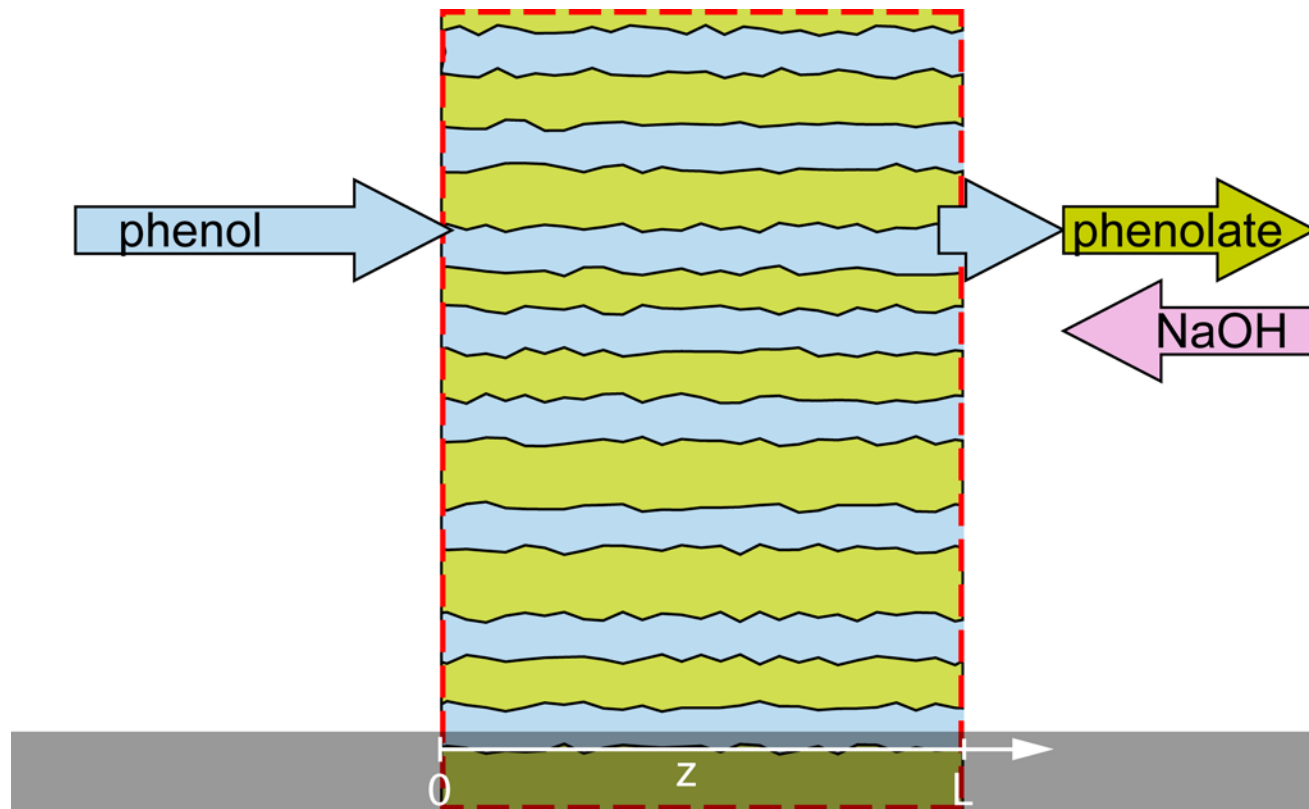
Boundary Conditions



Boundary Conditions



Boundary Conditions



- 6th boundary condition:

$$k_{mem} (c_{Phol}^{Feed} - c_{Phol}^{z=0}) \frac{c_{Phat}^{z=L}}{c_{Phol}^{z=L} + c_{Phat}^{z=L}} = D_{OH} \frac{\partial c_{OH}^{z=L}}{\partial z}$$

Numerical models and analytical solution (Olander)

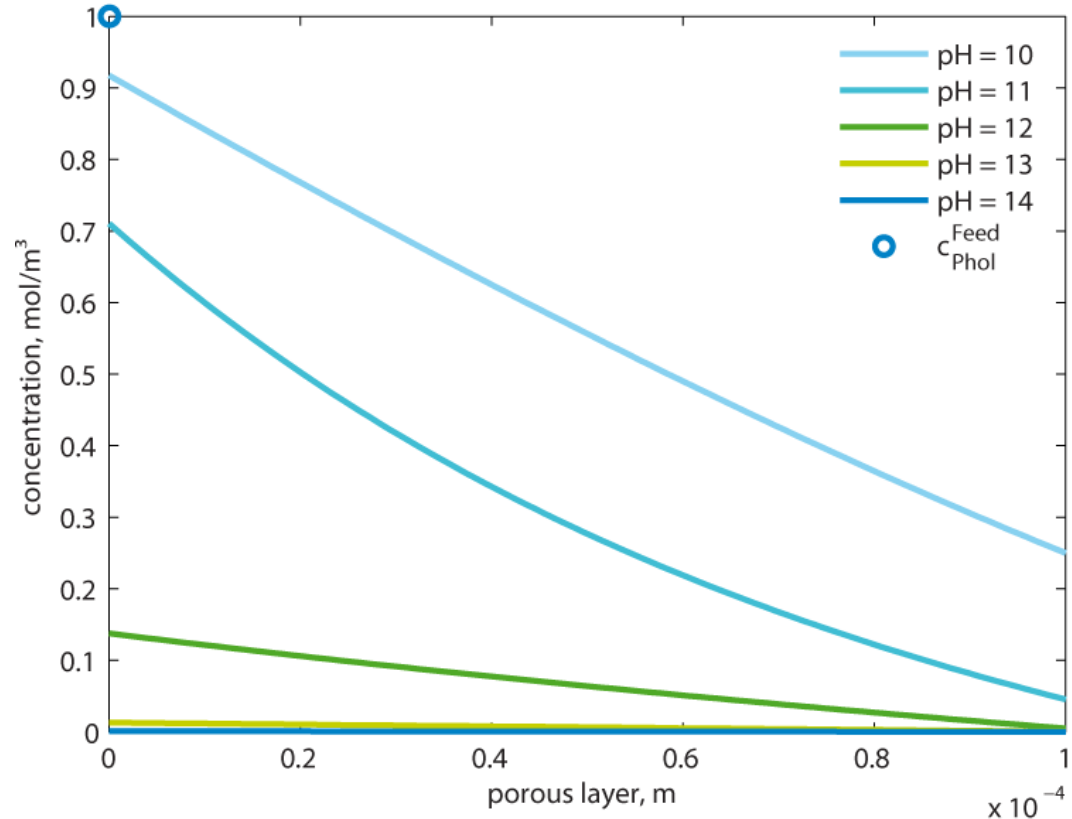
- Model for transmembrane phenol flow

$$\dot{n}_{Phol} = (c_{Phol}^{Feed} - c_{Phol}^{Perm}) \frac{1}{\frac{1}{k_{act}} + \frac{1}{E k_{por}}}$$

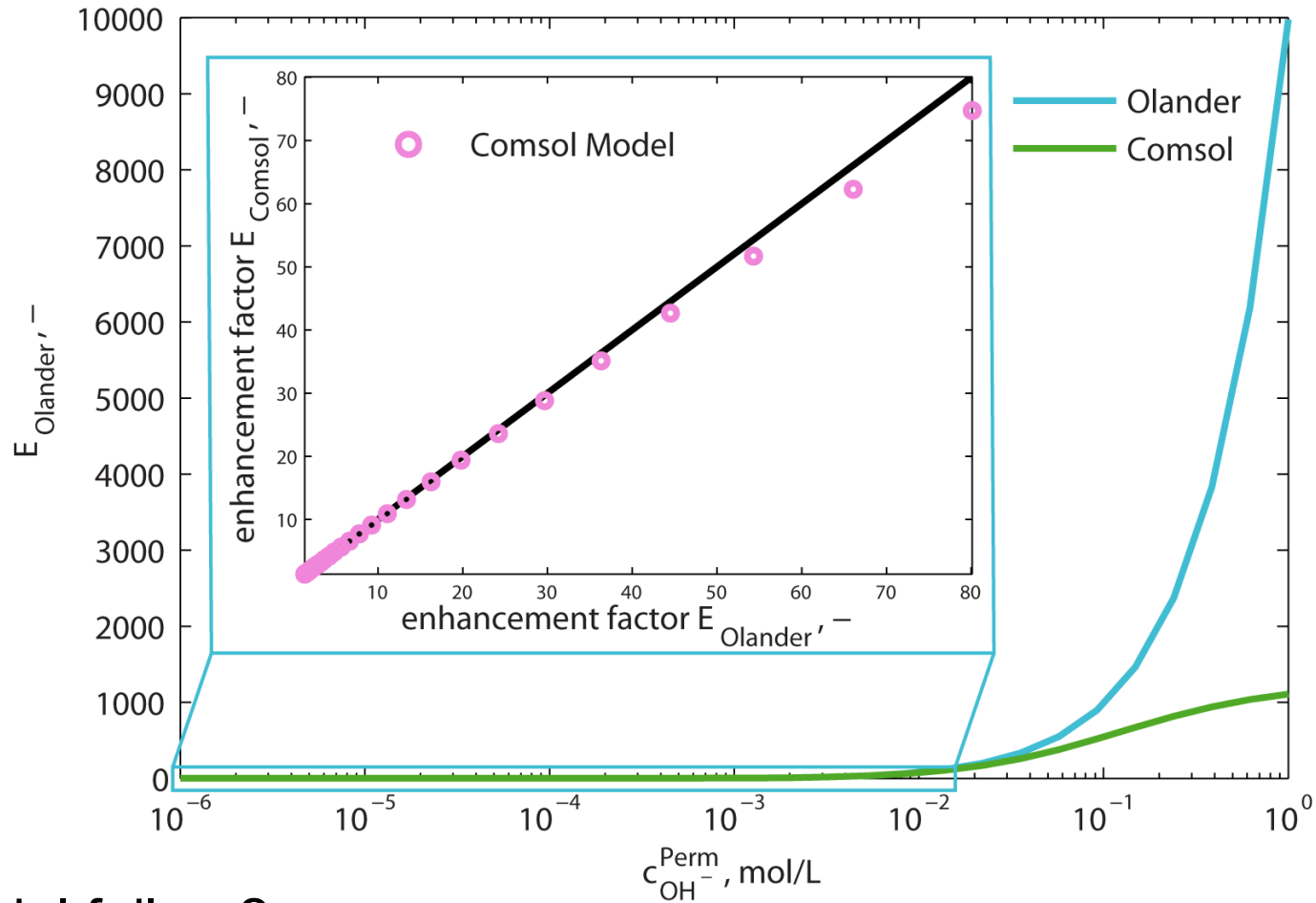
- Enhancement factor E dependent on chemical reaction
 - Can range from
 - 1, no improvement of extraction
 - ∞ , chemical reaction eliminates influence of porous structure
- Analytical solution for the calculation of E available
- Olander's solution acts as benchmark for Comsol

Comsol results, concentration profile

- Rising pH leads to reduced phenol-levels in the porous structure
- Higher phenol-difference across the dense layer with increased pH
- Caustic soda effectively reduces apparent thickness of porous layer

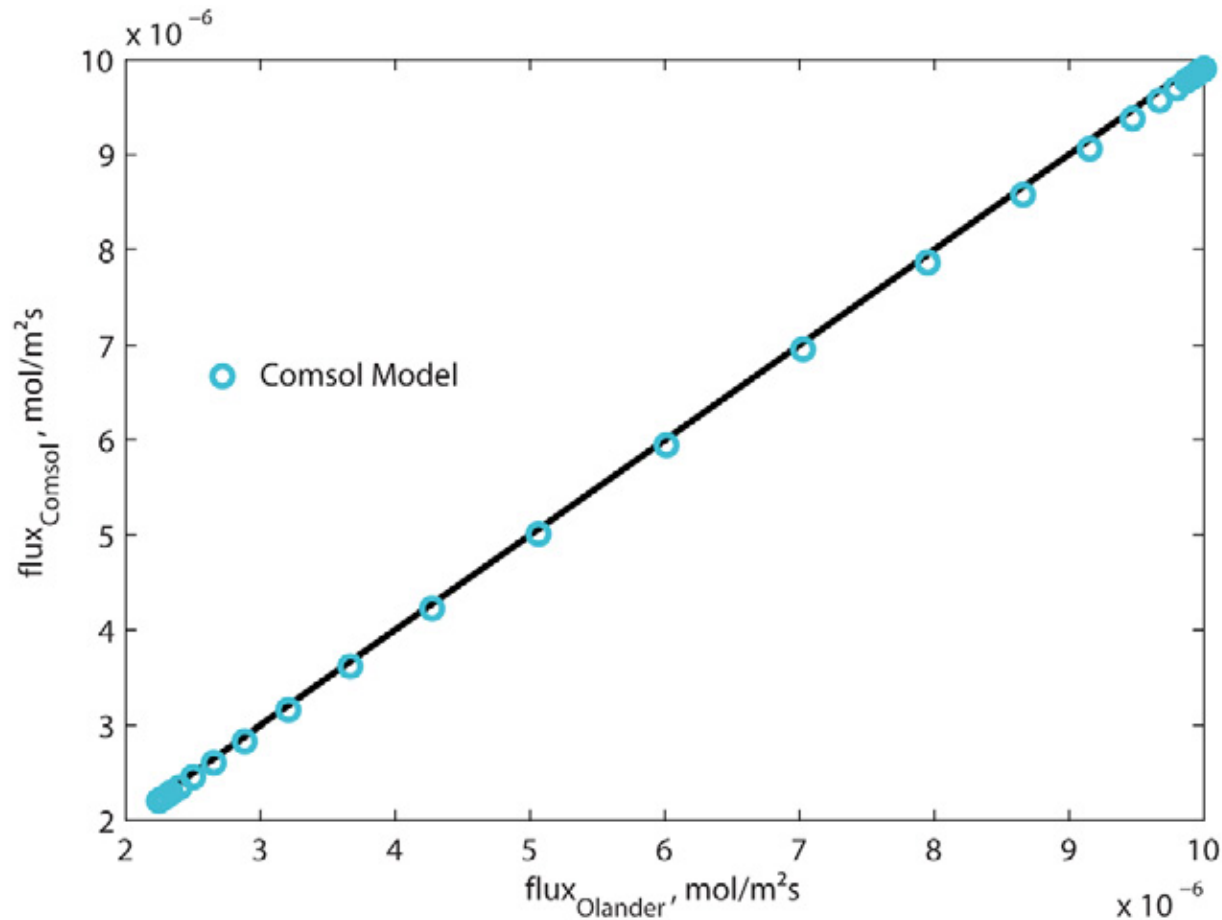


Model verification: Enhancement factor



→ Model failure?

Model verification: mass flow



→ Comsol model sufficiently accurate

→ E-factor of limited use

Summary and Outlook

- Lessons learned
 - Modeling of instantaneous reaction
 - shift from reaction rates to chemical equilibrium constant
 - Choice of boundary conditions
 - calculation of sodium hydroxide flow into the porous layer
 - Validation criteria
 - not as easy as it seems, validation by flow

- Outlook
 - Application of the model for the investigation of system parameters
 - Extension of the model to cover aspects like concentration polarization

AVT

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Thank you!

RWTH